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2 **Isolation, Identification and Production of Biobutanol by**
3 **Different *Clostridium* species Isolated from Soil Using**
4 **Waste Paper and Sugar Cane Molasses.**

5 **ABSTRACT**

6 Butanol as fuel component has some advantages compared to ethanol. The Study was
7 aimed at isolation of different types of *Clostridium* species from the soil and screening for
8 their capacity for production of bio-butanol. Soil samples were collected from three different
9 areas in keffi. Clostridium species were isolated using Reinforce Clostridial media and
10 identified using standard microbiological methods, mutation was induced in the *Clostridium*
11 isolates and 16s rRNA identification techniques was used to identify the isolates.
12 Quantitative screening of the *Clostridium* species isolates capacity in bio-butanol was carried
13 out using sugar cane molasses and waste paper substrate. The result using 16s rRNA
14 identification the *clostridium* isolated from old barracks was *C. acetobutylicium* the one
15 isolated from Amgwan kwara was *C. perfringenes* and *C. difficile* was isolated from Amgwan
16 Jaba. Screening for their bio-butanol producing capacity, it was observed that *C.*
17 *acetobutylicium* produces the highest before exposing to UV light to induce mutation with
18 9.61 ± 0.94 mg/l using sugar cane molasses and 4.89 ± 0.19 mg/l using waste paper followed
19 by *C. perfringenes* 6.24 ± 0.61 mg/l using molasses and 3.21 ± 0.11 mg/l using waste paper.
20 After exposing to UV light to induce mutation *C. acetobutylicium* produced 18.03 ± 0.17 mg/l
21 using molasses and 8.63 ± 0.06 mg/l using waste paper substrate follow by *C. perfringenes*
22 14.19 ± 0.11 mg/l and 5.99 ± 0.31 mg/l. From this study it was observed that *C.*
23 *acetobutylicium* has the capacity to produce bio-butanol and also inducing mutation will
24 enhance the capacity of *Clostridium* species in the production of bio-butanol.
25

26 **Key:** *Clostridium*, Bio-butanol, Molasses, Substrate

27 **1. Introduction**

28 The rate of energy demands combined with little resources of petroleum and environmental
29 condition have raised a new interest in production of renewable energy from biomass, such
30 as agricultural crops residuals, lignocellulosic waste and from industrial waste. Apart from
31 ethanol, butanol is superior in energy content, has lower volatility and is also less corrosive
32 to existing infrastructure [1]. There are three main areas remaining to be sorted out if bio-
33 butanol is to become a major counterpart in the bioenergy market. This includes optimizing
34 feedstock utilization, reaching theoretical maximum yields of butanol and minimizing energy
35 consumption during separation and purification [2].

36 One important driver for a bio-based economy is the exploitation of the bio-refinery concept
37 [3] where maximum value can be derived from the biomass through the generation of
38 multiple products and the effective use of process integration. Chemical pulp mills are
39 current examples of bio-refineries that can convert lignocellulosic biomass into energy, pulp,
40 cellulose derivatives, tall oil, etc. One strategy for mills to counteract competition from
41 tropical countries using fast-growing raw materials is to further expand the product portfolio
42 into additional value-added products. Cellulose is the primary fraction utilized for chemical
43 pulp production, while lignin, hemicellulose and extractives could be considered as by-
44 products in the process. Currently lignin and a portion of the hemicellulose, and the pulping
45 inorganics end up in the black liquor which is concentrated and burnt in a recovery boiler to

46 recover the chemicals and to supply energy for a large fraction of the mills process steam
47 requirements. Considering **the fact that** lignin has double the heating value as
48 polysaccharides, the hemicellulose fraction solubilized during alkaline pulping represents an
49 underutilized resource in many mills.

50 One option to enhance the value of the hemicellulose is to recover this fraction prior pulping
51 by using hot-water extraction [4, 5]. However, despite high yields of **xylene**, the removal of
52 hemicellulose from birch wood chips prior Kraft cooking has a negative impact of some pulp
53 properties affecting the quality of the paper. If a decrease in pulp strength properties cannot
54 be accepted, another option is to recover the **xylene** fraction from the black liquor.
55 Acidification of alkaline pulping liquors precipitates lignin as well as any hemicellulose
56 present in the liquor [6]. Technologies for recovery of lignin from Kraft liquors via CO₂
57 acidification has been the subject of pilot and demonstration-scale processes [7,8] with
58 proposed process of generating fuels, materials, and chemicals from the lignin as well as the
59 opportunity for “de-bottlenecking” capacity-limited recovery-boilers. Hemicelluloses are
60 typically degraded to **hydroxyl- acids** during Kraft pulping [9], although oligomeric **xylene**
61 from hardwoods may be more resistant to alkaline pulping than the glucomannans which are
62 the predominant softwood hemicelluloses due to the protection of glucuronic acid
63 substitutions against end-wise alkaline degradation, and as such, these **xylenes** may offer an
64 opportunity for recovery and utilization as a feedstock for bioconversion. In the present
65 study, the aim was to produce bio-butanol using waste paper by two clostridium species
66 isolated in soil of Keffi.

67 **2.0 MATERIAL AND METHODS**

68 **2.1 Study Area**

69 The study was carried out in Keffi, Nasarawa State, Nigeria. Keffi is approximately 68km
70 away from the Federal Capital Territory (FCT), Abuja and 128km away from Lafia, the capital
71 town of Nasarawa State. Keffi is located at longitude 8°5'E along the Greenwich Meridian
72 and at the equator and situated on longitude 850m above sea level [10].

73 **2.2 Sample Collection**

74 Three (3) soil samples were randomly collected (at the topsoil **5mm**) from three different
75 locations of Keffi metropolis such as Angwan Jaba, Old Barracks and Angwan kwara using a
76 clean spoons and stored using disposable screw bottle and transported immediately to the
77 Microbiology Laboratory, Nasarawa State University, Keffi for isolation.

78 **2.2.1 Isolation of *Clostridium* species**

79 The isolation of *Clostridium* species from three **different** areas in Keffi was carried out using
80 spread plate method. One (1.0g) of the soil sample was suspended in 9.0ml of sterile
81 distilled water containing tween 80 and 7 folds dilutions were made and 0.1ml of the aliquot
82 was spread on petri dishes of freshly prepared Reinforce Clostridial media containing yeast
83 extract 3.0; lab-lemco powder 10.0; peptone 10.0; soluble starch 1.0; glucose 5.0; cysteine
84 hydrochloride 0.5; sodium chloride 5.0, sodium acetate 3.0 and agar agar 1.0. Incubated in
85 anaerobic jar at 37°C for 48 hours.

86 **2.1.3. Identification of *Clostridium* species**

87 Cultural and morphological identifications of *Clostridium* species were carried out in
88 accordance with Bergey's Manual of Determinative Bacteriology [11] such as swarming test,
89 gram staining test, endospore Staining egg yolk agar test, nagler test, lipase test Indole test,
90 catalase test and urease test.

91 **2.1.4 Hank's Buffer/UV light treatment of *clostridium* isolates**

92 **Induction** of mutation in *Clostridium* isolates was carried out by the modification of a method
93 described by [12]. *Clostridia* isolates were grown on Reinforce Clostridial medium
94 **maintained** in Hank's buffer (137mM NaCl, 5.4mM KCl, 4.4mM KHIO₄, 0.33mM Na₂HPO₄,
95 1.3mM CaCl₂, 0.81mM MgSO₄, 4.2mM NaHCO₃, 1g/L glucose, pH 7.4) and were
96 subsequently exposed for 1 hour to ultra violet light rays from 2 white fluorescent tubes (TFC
97 FL-20 SD/18W Day Light). Isolates were exposed at a distance of 15cm. isolates were
98 added to a mixture of 75% methanol and 25% acetic acid for 1 hour. The isolates were
99 subsequently incubated in 70% ethanol containing 0.07N NaOH overnight at 4 °C. Isolates
100 were analyzed using 16S rRNA gene sequencing for identification.

101 **2.1.5 Extraction of bacterial DNA for 16S rRNA gene sequencing**

102 Eighty (80 µl) of NaOH (0.05M) was added to 20 µl of *Clostridium* isolates, were suspended
103 in distilled water and the mixture was incubated at temperature of 60C for 45 minutes, 6 µl
104 of Tris/HCl (pH 7.0) were addition to achieve a final pH of 8.0. The mixture was diluted by
105 ×100 and 5 µl of the diluted extract was used for the polymerase chain reaction (PCR).

106 **2.1.6 PCR, gel electrophoresis, and 16S rRNA gene sequencing**

107 Treated distilled water DNase I and PCR master mix (containing dNTPs, PCR buffer, and
108 Taq polymerase) were used in all PCR reactions by adding 1 U of DNase I (Pharmacia,
109 Uppsala, Sweden) to 40 µl of distilled water or PCR master mix, the mixture was incubated
110 at 25°C for 15 minutes, and later at 95°C for 10 minutes to inactivate the DNase I. The
111 clostridial isolates, DNA extracts and control was amplified with 0.5µM primers (27F, 5'-
112 TGGCGAACGGGTGAGTAA-3' and 1525R, 5'-AGGCCCGGGAACGTATTCAC-3'; Inqaba
113 Biotechnical Industries (Pty) UK). The PCR mixture (50 µl) contained *Clostridium* isolates
114 DNA, PCR buffer (10mM Tris/HCl (pH 8.3), 50mM KCl, 2mM MgCl₂, and 0.01% gelatin), 200
115 µM of each dNTP, and 1.0 U Taq polymerase (Boehringer Mannheim, Mannheim,
116 Germany). The mixtures were amplified by 40 cycles of 94°C for one minute, 55°C for one

117 minute, and 72°C for two minutes, with a final extension at 72°C for 10 minutes in an
118 automated 0.5 ml GeneAmp PCR system 9700 (Applied Biosystems, Foster City, California,
119 USA). DNase I treated distilled water was used as the negative control. A 10 µl aliquot of
120 each amplified product was electrophoresed in 1.0% (wt/vol) agarose gel, with a molecular
121 size marker (λ DNA Avall digest; Boehringer Mannheim) in parallel. Electrophoresis in
122 Tris/borate/EDTA buffer was performed at 100 V for 1.5 hours. The gel was stained with
123 ethidium bromide (0.5 µg/ml) for 15 minutes, rinsed, and photographed under ultraviolet light
124 illumination.

125 The PCR products were gel purified using the techniques developed by the National Centre
126 for Bioinformatics, Islamabad, Pakistan. Both strands of the PCR products were sequenced
127 twice with an ABI 377 automated sequencer according to the manufacturers' instructions
128 (Inqaba Biotechnical Industries (Pty) Ltd UK) using the PCR primers (27F and 1525R).

129 **2.1.7 The pre-treatment of waste papers**

130 The pre-treatment of waste papers was carried out as **described** by [13]. The waste papers
131 were thoroughly washed in water to remove dust. Waste paper substrates were pre-treated
132 with 3% NaOH for 1 hour. Then, they were washed and neutralized with 0.1N HCl at pH 5.
133 The pre-treated waste papers were dried at 45 °C in an oven after neutralization.

134 **2.1.7.1 Acid hydrolysis**

135 Acid hydrolysis was done to break down cellulose into glucose units. It was carried out by
136 soaking 10g of paper in different amounts of sulfuric acid 5%: 100, 200 and 300 ml of water
137 for 2 hours. The mixture was autoclave at 121°C. After hydrolysis, the samples were filtered
138 and centrifuged to obtain the hydrolysate product. The pH of the obtained product was
139 adjusted to 5.0 by adding sodium hydroxide solution 5M

140 **2.1.8 Preparation of Molasses**

141 The preparation of molasses from sugarcane was carried out as described by [14, 15]. The
142 sugarcane was stripped off leaves. Its juice was extracted by cutting, crushing and mashing.
143 The juice was boiled over a Bunsen burner to concentrate it, promoting sugar crystallization.
144 The product of this first boiling called first syrup was used as a component of the
145 fermentation medium.

146 **2.1.9 Quantitative Analysis of Reducing Sugar Present in Fermentation medium**

147 The quantitative analysis was carried out using 3, 5–dinitrosalicylic acid. The concentration
148 of the sugar present in the samples was determine by adding 1cm³ of 3, 5-dinitrosalicylic
149 acid to 1cm³ of each of the samples and boiled for 5 minutes and 10cm³distille water was
150 added. The absorbance of each of sample was determined at 540nm using JENWAY 6400

151 spectrophotometer. Thus, the concentration values were extrapolated from the glucose
152 standard curve

153 **2.1.10 Preparation of inoculum**

154 The seed culture was carried out as described by [16]. The cultivated organism two colonies
155 was inoculated into 10 ml of Reinforce Clostridial broth and incubated in an anaerobic jar at
156 37 °C for 6 hours.

157 **3.0 Production of Bio-butanol**

158 **3.1 Fermentation**

159 The batch fermentation was carried out as earlier described by [17] with modification. The
160 100 ml from the starter culture was inoculated in 900 ml of fermentation media
161 (enzymatically hydrolyzed waste papers and molasses) containing 25g of sugar. The
162 fermentation media were incubated under strict anaerobic and sterile conditions at 35°C for
163 96 hours.

164 **3.1.2 Extraction and purification of bio-butanol from fermentation broth**

165 Extraction and purification of solvents from the fermentation broth were carried out using a
166 modification of the method described by [13]. In this method, *Clostridium* species were used
167 in the fermenter. The extracting solvent was an alkylate which was substantially free from
168 impurities and had a boiling range of 118°C. The apparatus for carrying out the process
169 included a standard fermenter receiving fermentation broth including a carbon source and
170 microorganisms at a feed stream which are agitated and maintained at a desired
171 fermentation temperature. The butanol-containing broth was drained through a first stream
172 discharging into the upper end of an extraction column where it flowed downwardly through
173 the extractor. A second stream released a light alkylate into the bottom of the column for
174 upward countercurrent flow relative to the downward flow of the broth. The light alkylate was
175 fed from an alkylate source stream, separated in a splitter with the light end boiling in the
176 range of 1 °C. The butanol containing alkylate extract was discharged through a stream at
177 the top of the extractor to flow through a dryer (a desiccator), in order to purify it and remove
178 any excess water content. The extraction was carried out at a steady state with a solvent
179 feed ratio ranging from 5–20 ml. The solvent was removed through the column at a rate of
180 200 – 450 ml per minute.

181 **3.1.3 Separation and quantification of bio-butanol**

182 The separation and quantification of bio-butanol produced by *Clostridium* species were
183 carried out by Gas Chromatography and Mass Spectrometry (GC & MS) as described by
184 [13]. One microliter (1.0 µL) of acidified sample was injected into “SHIMAZU GC-14, Gas
185 Chromatograph” equipped with flame-ionization detector.

186 The column used for the separation of solvent was PEG (2.1m x3.0mm). The temperature
187 programming of the column oven was 60 °C/min. One hundred and twenty degrees
188 centigrade (120 °C), Nitrogen gas (30 mL/minutes) was used as carrier gas. The
189 temperatures of injector and detector were 150 °C and 200 °C respectively. The Peaks were
190 recorded on “SHIMADZU C-R-4_A, Chromatograph”, and were identified by comparison of
191 the retention times with that of standard mixture. The experiment was carried out in
192 duplicates and the means ± standard deviations of the yield of butanol were recorded. The
193 standard calibration curve presented was used in calculating the concentration of bio-butanol
194 produced by the various *Clostridium* isolates.

195 3. Results

196 The species of *Clostridium* that were isolated from soil in Keffi were identified using Cultural,
197 Morphology and different biochemical test as given in table 1. The three species of
198 *Clostridium* isolated from different location in Keffi was able to produce bio-butanol after
199 screening for bio-butanol production at pH 5.5, temperature of 37°C for 96hours were
200 *Clostridium* specie isolated from Old barracks produced the highest butanol 9.61± 0.94 mg/l
201 using sugar cane molasses and sugar utilization of 9.61±0.71 g/l and 4.8±0. 19mg/l using
202 waste paper substrate followed by *Clostridium* species isolated from Angwan Jaba 6.21±
203 0.61 mg/l, 9.05±1.11 g/l of sugar utilization using molasses and 3.21 ± 0.11 mg/l using waste
204 paper substrate *Clostridium* isolated from Angwan kwara 5.48±0.99 mg/l and 10.11± 0.99 g/l
205 of sugar utilization sugar cane molasses and 1.97 ± 0.33 mg/l using waste paper substrate.
206 Mutation was induced in the *Clostridium* isolates and were identify using 16s rRNA as shown
207 in figure 1, 2 and 3 respectively. bio-butanol produced pH 5.5, temperature of 37°C for
208 72hours after the induce of mutation as given in table 2 using waste paper as fermentation
209 substrate shows that *Clostridium* species isolated from old barracks was *C. acetobutylicum*
210 also produce the highest butanol after mutation with 8.63±0.06 mg/l sugar utilization of
211 6.21±0.11 g/l followed by *C. perfringenes* isolated from Amgwan kwara 5.99 ± 0.31 mg/l,
212 sugar utilization of 4.89±0.19 g/l and *C. difficile* isolated from Angwan Jaba 3.01± 0.54 mg/l
213 and sugar utilization of 3.97±0.33 g/l respectively. Table 3 shows bio-butanol produced using
214 sugar cane molasses by the *Clostridium* isolates were *C. acetobutylicum* produced highest
215 16.63±0.06 mg/l and sugar utilization of 16.98±0.51 mg/l followed by *C. perfringenes* 14.19 ±

216 0.11mg/l sugar utilization of 12.99±0.06 mg/l and the lowest was produced by *C. difficile*
 217 10.01± 0.01mg/l and 9.89±0.19 mg/l utilization of sugar respectively.

218 Figure 1, 2 and 3 shows the phylogenetic tree of the different species of the *Clostridium*
 219 isolated from different location.

220 **Table1. Cultural, Morphology and Biochemical Characteristics Test**

	Cultural Morphology characteristics								Inference
	Gram stain	Endo	Egg york test					Spore	
			lipase	NR	LE	cat			
			IND						
			UV	Sg/UV					
Glossy, grey	-	+	-	+	+	-	+	<i>C. difficile</i>	
Large smooth	-	+	Nil	Nil	-	-	-	<i>C. perfringenes</i>	
Raised	-	+	+		-	-	-	<i>C. acetobutylicium</i>	

221 Key: UV fluorescence , NR- No reaction, SW- swarming growth, LE- Lecithinnase. Cat-
 222 catalase, IND- indole.

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227 **Table2: Bio-butanol produced by different *Clostridium* isolates before mutation at**
 228 **pH5.5, 37°C after 96hours**

Isolates	Initial sugar concretion (g/l)	Sugar utilization (g/l)	Bio-butanol produced using waste paper (mg/l)	Bio-butanol produced using sugar cane molasses (mg/l)
Clostridium (AJ)	20	9.05±1.11	3.21±0.11	6.21±0.61
Clostridium (AK)	20	10.11± 0.04	1.97±0.33	5.48±0.99
Clostridium (OB)	20	9.61±0.71	4.89±0.19	9.61± 0.94

229 Key: AJ= Angwan Jaba, AK= Amgwan kwara, OB= Old barracks

230 **Table3: Bio-butanol produced by different *Clostridium* isolates after mutation at**
 231 **pH5.5, 37°C after 96 hours**

Isolates	Initial sugar (g/l)	Sugar utilization (g/l)	Bio-butanol produced using waste paper (mg/l)
<i>C. acetobutylicium</i>	20.1±0.50	6.21±0.11	8.63±0.06
<i>C. difficile</i>	20.1±0.50	3.97±0.33	3.01± 0.54
<i>C. perfringenes</i>	20.1±0.50	4.89±0.19	5.99 ± 0.31

232

233 **Table 4: Bio-butanol produced by different clostridium isolates after mutation at**
 234 **pH5.5, 37°C after 96 hours**

Isolates	Initial sugar (g/l)	Sugar utilization (g/l)	Bio-butanol produced using sugar cane molasses (mg/l)
<i>C. acetobutylicium</i>	25.01±0.50	16.98±0.51	18.03±0.17
<i>C. difficile</i>	25.01±0.50	9.57±0.93	10.01± 0.01

C. perfringens

25.01±0.50

12.99±0.06

14.19 ± 0.11

235



236

237 **Figure 1: Phylogenetic Tree of the Molecular Characterization of *Clostridium***
238 ***acetobutylicum* isolated from old Barracks Keffi.**



Figure 2: Phylogenetic Tree of the Molecular Characterization of *Clostridium difficile* isolated from Angwan Jaba in Keffi.



242

243 **Figure 3: Phylogenetic Tree of the Molecular Characterization of *Clostridium***
 244 ***perfringens* isolated from Angwan kwara in Keffi**

245 **4. Discussion**

246 Butanol as fuel or blending component has some advantages compared to ethanol. For
 247 example a lower vapour pressure and higher energy density. The production of butanol in a
 248 microbial fermentation was first reported by Pasteur in 1861. Three different species of
 249 clostridium were isolated and identified using 16s rRNA from different location from soil in
 250 Keffi, were *C. perfringens*, *C. difficile* and *C. acetobutylicum*. This however, is not in contrary
 251 with studies earlier reported by [18] that *Clostridium* species are one of most common
 252 bacteria isolated from the soil environment. Bio-butanol production by different species of
 253 *Clostridium* isolated in this study is in agreement with other studies earlier described by [19,
 254 20, 21] that *Clostridium* species are some bacteria that has the ability in production of bio-
 255 butanol. In the study it was observed that *Clostridium* species isolated from old barracks has
 256 the highest accumulation of bio-butanol at 37°C, pH5.5 after incubation of 96 hours.
 257 Fermentation parameters and type of fermentation substrate play an important role in
 258 production of bio-butanol. It was observed that were was high production of bio-butanol

259 using sugar cane molasses and glucose which contain noncomplex sugar than using waste
260 paper which is made up of lignin which need to be detoxified to enhance the used of waste
261 paper in the production of bio-butanol to remove the inhibitor that will affect the growth of the
262 *Clostridium* isolates as earlier reported by [22]. In this study it was observed that the sugar
263 cane molasses has higher yield of bio-butanol that when used in a media containing the
264 waste paper, also base on the isolates that yield has the highest accumulation of the bio-
265 butanol it observed that *C. acetobutylicum* has the accumulation of 8.63±0.06 mg/l in use of
266 waste paper as substrate and 18.03±0.17 mg/l on sugar cane molasses as substrate which
267 is agreement with work earlier reported by[18]. Also it was observed that there was increase
268 in the production of biobutanol after the isolate was expose to UV light for mutation which
269 suggested that for economical bio-butanol production using *Clostridium* species, Induction of
270 mutation will enhance the production of bio-butanol industrially

271

272 5. Conclusion

273

274 *Clostridium* species isolated from soil environment showed high capacity of production of
275 bio-butanol. It was observed that the use of both molasses and waste paper will be a good
276 source of carbon or media in the production of bio-butanol. Inducing mutation in *Clostridium*
277 species will help to overcome the challenges of using clostridium in industrial scale
278 production of bio-butanol.

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