

STUDY OF BIO SORBENTS FOR THE TREATMENT OF SIMULATED DYES WASTE WATER

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Abstract

Environmental contamination is one of the burning issues of today's world. Pollution not only causes environmental changes but also causes different diseases. Textile effluent is a major contributor of water pollution. Marine lifespan, environment and our ecosystem are affected severely by the disposal of dyes from industries into the receiving water. The objective of this research is adsorption, thermodynamics and kinetic studies of two different organic dyes onto abundantly available inexpensive adsorbents like *Phoenix dactylifera* (date pits), *tea waste* (tea leaves), *Zea covering* (corn husk) and *Prunus persica* (peach seeds) for the elimination of acidic (Congo red) and basic (Malachite Green oxalate) dyes from solutions. Selected adsorbents have high surface reactivity and adsorption capability to eliminate malachite green oxalate dye and Congo red dye respectively from simulated waste water system.

INTRODUCTION

Rapid industrialization has seriously contributed to the release of toxic dyes to water streams. It is well known that malachite green oxalate and congo red, are highly toxic dyes, considered as priority pollutants. These dyes are often discharged in a number of industrial processes, especially manufacturing batteries, electroplating, pigments and ammunition production, which can lead to water contamination in turn. Dyes are not biodegradable and tends to accumulate in living organisms causing diseases and disorders [1]. Therefore, removal of dyes from wastewater is currently one of the most important environmental issues being investigated. Treatment processes of malachite green oxalate and congo red dye removal from wastewater through adsorption have recently been studied [2]. However, it has become a challenge for researchers to seek cheaper and more effective adsorbents for dyes removal.

Tea leaves, corn husk, date pits and peach seeds are the most widely consumed products throughout the world for its beneficial effects on health, such as antioxidant, anti-carcinogenic, antimicrobial activities [3]. The objectives of the present study are to evaluate the removal of congo red dye with treated tea residue and with date pits and the removal of malachite green oxalate dye with corn husk and peach seeds because these mentioned adsorbents adsorb 99% dyes from waste water. All natural adsorbents were originate to be reliant on contact time, dye concentration and dose of adsorbent by using spectrophotometric technique before and after dye adsorption. Maximum adsorption of date pits occurred in 20 min with percentage removal of 96.3 %, maximum adsorption of tea leaves ensued in 30 min with 94.23%, extreme adsorption of peach seed powder happened in 40 min with 95.48%, the best adsorption of corn husk arisen in 40 min with 94.40%. The percentage dye removal would decrease with increase in dye concentration, whereas the adsorption capacity of adsorbents will increase with increase in the dye concentration. The investigational data fitted well to pseudo second order kinetics model and have a Regression coefficient value of 0.999 approximately [4]. Values of percentage removal and K_D for all the adsorbents and dyes systems were also determined at temperatures ranging from 298K to 318K. The adsorption isotherms like Langmuir and Freundlich were employed and the values of respective constants were calculated to estimate the adsorption characteristics [5]. Several thermodynamic parameters like ΔG° , ΔH° and ΔS° were also calculated and it was observed that adsorption is spontaneous and endothermic. Pseudo-second order simulations were used to define the dyes adsorption kinetics. The adsorption equilibrium data were fitted well to adsorption isotherm models and proved the pseudo-second order adsorption kinetics [6]. The surface morphology of adsorbate and adsorbent was resolute by SEM technique of Jeol Japan with model number JSM 6380A. The liquid phase is then analyzed for the equilibrium concentration C_e of the chemical in aqueous solution. **K_D (the adsorption–desorption coefficient)** values are determined over a range of concentrations at a constant temperature [7]. The resultant plot is termed an **adsorption** “isotherm”, which can take a number of shapes as illustrated below from figure 1 to 8.

EXPERIMENTAL SECTION

Preparation of malachite green oxalate and congo red dye Solutions

Dye solution of congo red was prepared by using double distilled water. The absorbance of respective concentrations of dye was measured by UV-Visible spectrophotometer of Jeol Japan with model number EX-54175JMU displays a penetrating peak in diluted concentration of dye around 498 nm in aqueous solution. Molar extinction coefficient of congo red is approximately 45000 l/mol.cm. Similarly Malachite green oxalate dye displays a penetrating peak in diluted concentration of dye around at wavelength 621 nm and its molar extension coefficient is $1 \times 10^5 \text{ M}^{-1} \text{ cm}^{-1}$ [8-10].

Preparation of natural adsorbents

Peach, corn, tea and date wastes were collected from Nazimabad suburb of Karachi, Pakistan, washed with distilled water, ground and sieved into powder of sizes 0.146-0.342 mm, 0.1546-0.4623 mm and 0.0365-0.2876 mm, 0.265-0.435 mm, respectively dried in an oven at 390 K for 2 days, after complete drying all adsorbents were stored in desiccator for further use.

Optimization of adsorbent dosage

For the analysis of maximum adsorption, which occurs at the ideal amount of peach seeds, experimentation was accomplished. For this tenacity, 30.0 ml of MGO dye with concentration $3 \times 10^{-5} \text{ mol.dm}^{-3}$ was taken, different amount was taken from 0.1g -1.2g. All the flasks were placed on shaking in a thermostat shaker for 30 min. After the shaking all the flask were filtrated out by Wattman filter paper and first 10 ml of filtrate was thrown away. Filtrate of each flak examined by UV visible spectrophotometer for detecting absorbance after adsorption process of each solution.

Dissimilar amount of corn husk from 0.1g-1.2g were measured and put into the conical flask having 30ml of $5 \times 10^{-5} \text{ M}$ solution of MGO dye and placed at the hot plate for 30 minutes. After 30minutes final absorbance was examined by UV-visible spectrophotometer for measuring the absorbance of solution at 617 nm. In this way the value of finest amount was determined at which extreme adsorption occurred.

1×10^{-5} M solution was prepared. Different amount of tea leaves waste 0.1g to 0.8g was measured and placed in respective conical flasks. 25ml of 1×10^{-5} M solution was drawn in the flask. After 30min final absorbance was analyzed by UV visible spectrophotometer at 496nm. In this way ideal amount was determined at which extreme adsorption occurred.

Optimization of pH Of Point Zero Charge (Ph_{pzc})

The pH of Point Zero Charge (pH_{PZC}) was determined by adopting pH drift method for the efficient removal of dyes solution. The 0.005M NaCl solution was prepared and initial pH was adjusted by adding either 0.1M HCl or 0.1M NaOH in such a manner that 3 flasks have acidic pH (2, 4, and 6) and other 3 flasks have basic pH (8, 10, 12). The solutions were agitated with 0.05g of adsorbents and pH was recorded. pH of flasks were noted after 24 and 48hr .

Ionic Strength (KCl)

Different concentrations of KCl (0.01–0.05 M) were added to investigate the effect of ionic strength for the adsorptive removal of dyes. The increase in ionic strength causes increase in the adsorption of congo red and malachite green oxalate dye.

Determination of shaking time

For determining the maximum time of adsorption for each natural adsorbent, 30ml with 3×10^{-5} M for the powder of peach seeds cover and dye solutions were taken out in reagent bottles. Best amount of adsorbent was taken which was determined in preceding experiment in every flask. These flasks were placed in a shaking incubator and after every 5 minutes one bottle was removed from the incubator. Solution was filtered and examined with UV visible spectrophotometer in order to recognize absorbance of solution after dissimilar shaking time intermissions. Optimal shaking time for the adsorption was 30 minutes for all bottles.

Optimized amount of corn husk 0.5g was measured and put into the conical flask with 30ml of 5×10^{-5} M solution concentration of malachite green for different time interval after respective particular time, final absorbance was measured at 617 nm. The time where maximum adsorption occurred was taken as optimum time for adsorption [11]. Optimum amount of tea leaves waste 0.5 g was measured and placed in column with 30ml of 1×10^{-5} M concentration solution of congo

red for different time of interval after respective particular time. Final absorbance was measured at 496nm. The time where maximum adsorption occurred was taken as optimum time for adsorption. Optimum amount of date pits waste 0.6 gm was measured and placed in column with 30ml of $1 \times 10^{-5} \text{M}$ concentration solution of Congo red for different time of interval after respective particular time. Final absorbance was measured at 496nm. The time where maximum adsorption occurred was taken as optimum time for adsorption.

Optimization of adsorbate concentration

Working standard of dye solutions were prepared by varying the concentrations of 50ml of each nano particle solution and 30ml of each of natural adsorbents were taken in separate flask and optimized amount of adsorbent was added in respective flask and kept them in shaking incubator by keeping optimized time at 303K temperature. After optimized time the contents were filtered out and absorbance of each the content was measured at their respective λ_{max} . The optimum range of concentration of MGO and CR dyes were selected for further studies [12].

TABLE 1: ANALYSIS OF AMOUNT

| Optimization of Amount for the Elimination of Congo Red Dye by Using Tea leaves powder | | | |
|---|-------------------------------------|-----------|--------|
| Amount(g) | Equilibrium Conc. $\times 10^6$ (M) | % Removal | K_D |
| 0.1 | 2.933 | 93.139 | 1.761 |
| 0.2 | 1.842 | 77.452 | 1.751 |
| 0.3 | 9.111 | 78.690 | 1.822 |
| 0.4 | 4.066 | 90.488 | 0.612 |
| 0.5 | 7.601 | 82.224 | 0.912 |
| 0.6 | 9.602 | 77.546 | 0.961 |
| 0.7 | 2.977 | 93.035 | 0.255 |
| 0.8 | 2.466 | 94.230 | 0.185 |
| Optimization of Amount for the Elimination of Congo Red Dye by Using Date pits powder | | | |
| Amount(g) | Equilibrium Conc. $\times 10^7$ (M) | % Removal | K_D |
| 0.1 | 0.213 | 67.123 | 128 |
| 0.2 | 6.888 | 89.383 | 20.666 |
| 0.3 | 0.153 | 76.369 | 30.666 |
| 0.4 | 0.106 | 83.561 | 16 |
| 0.5 | 3.333 | 94.863 | 4 |
| 0.6 | 2.444 | 96.232 | 2.444 |

| 0.7 | 6.444 | 90.068 | 5.523 |
|--|---------------------------------------|-----------|----------------|
| 0.8 | 7.555 | 88.356 | 5.666 |
| 0.9 | 4.222 | 93.493 | 2.814 |
| Optimization of Amount for the Removal of MGO Dye by using Corn Husk powder | | | |
| Amount(g) | Equilibrium Conc.x10 ⁶ (M) | % Removal | K _D |
| 0.1 | 1.712 | 89.579 | 10.275 |
| 0.3 | 1.141 | 93.052 | 2.283 |
| 0.5 | 9.200 | 94.401 | 1.104 |
| 0.7 | 1.423 | 91.336 | 1.220 |
| 0.9 | 1.920 | 88.312 | 1.280 |
| 1.2 | 1.631 | 90.069 | 0.815 |
| Optimization of Amount for the Removal of MGO Dye by Using Peach seeds shell powder | | | |
| Amount(g) | Equilibrium Conc.x10 ⁶ (M) | % Removal | K _D |
| 0.1 | 0.210 | 89.605 | 4.905 |
| 0.3 | 0.152 | 90.134 | 5.081 |
| 0.5 | 8.193 | 94.697 | 1.638 |
| 0.7 | 7.051 | 95.436 | 1.007 |
| 0.9 | 8.193 | 94.697 | 0.910 |
| 1.2 | 6.984 | 95.480 | 0.582 |

TABLE 2: ANALYSIS OF TIME

| Optimization of time for the Elimination of CR Dye by Using Tea leaves powder | | | | |
|--|------------|--|-----------|----------------|
| Amount(g) | Time (min) | Equilibrium Concentration(C _e)x10 ⁶ | % Removal | K _D |
| 0.5 | 10 | 1.991 | 53.430 | 2.389 |
| 0.5 | 15 | 4.933 | 88.461 | 0.592 |
| 0.5 | 20 | 1.468 | 65.644 | 1.762 |
| 0.5 | 25 | 4.888 | 88.565 | 0.586 |
| 0.5 | 30 | 2.466 | 94.230 | 0.296 |
| 0.5 | 35 | 2.133 | 95.010 | 0.256 |
| 0.5 | 40 | 2.111 | 95.062 | 0.253 |

| 0.5 | 45 | 2.133 | 95.010 | 0.256 |
|--|------------|---|-----------|----------------|
| Optimization of time for the Removal of CR Dye by Using Date pits powder | | | | |
| Amount(g) | Time (min) | Equilibrium Concentration(Ce)x10 ⁷ | % Removal | K _D |
| 0.6 | 10 | 6.889 | 89.383 | 6.888 |
| 0.6 | 15 | 5.333 | 91.780 | 5.333 |
| 0.6 | 20 | 1.776 | 97.260 | 1.777 |
| 0.6 | 25 | 2.221 | 96.575 | 2.222 |
| 0.6 | 30 | 2.454 | 96.232 | 2.444 |
| 0.6 | 35 | 1.911 | 70.547 | 19.111 |
| 0.6 | 40 | 1.012 | 81.506 | 12.000 |
| 0.6 | 45 | 9.551 | 85.273 | 9.555 |
| 0.6 | 50 | 4.667 | 92.808 | 4.666 |
| Optimization of time for the Removal of MGO Dye by Using Corn husk powder | | | | |
| Amount(g) | Time (min) | Equilibrium Concentration(Ce)x10 ⁶ | % Removal | K _D |
| 0.5 | 10 | 1.296 | 92.112 | 1.555 |
| 0.5 | 15 | 1.182 | 92.807 | 1.418 |
| 0.5 | 20 | 1.081 | 93.420 | 1.297 |
| 0.5 | 25 | 1.141 | 93.052 | 1.370 |
| 0.5 | 30 | 9.402 | 94.278 | 1.128 |
| 0.5 | 35 | 1.141 | 93.052 | 1.370 |
| 0.5 | 40 | 8.596 | 94.769 | 1.031 |
| 0.5 | 45 | 8.730 | 94.687 | 1.047 |
| 0.5 | 50 | 1.148 | 93.011 | 1.378 |

| Optimization of time for the Removal of MGO Dye by Using peach seeds powder | | | | | |
|--|-------------------------|------------|--|-----------|--------------------|
| S. No. | Amount Of Adsorbent (g) | Time (min) | Equilibrium Concentration Ce (M)x10 ⁷ | % Removal | K _D (M) |
| 01 | 0.7 | 10 | 5.104 | 96.697 | 0.729 |
| 02 | 0.7 | 15 | 4.499 | 97.088 | 0.642 |
| 03 | 0.7 | 20 | 8.260 | 94.654 | 1.1801 |
| 04 | 0.7 | 25 | 7.051 | 95.436 | 1.007 |
| 05 | 0.7 | 30 | 7.051 | 95.436 | 1.009 |
| 06 | 0.7 | 35 | 5.036 | 96.740 | 0.719 |
| 07 | 0.7 | 40 | 3.492 | 97.740 | 0.498 |

| | | | | | |
|----|-----|----|-------|--------|-------|
| 08 | 0.7 | 45 | 5.439 | 96.479 | 0.777 |
|----|-----|----|-------|--------|-------|

| TABLE 3: ANALYSIS OF TEMPERATURE | | | | | |
|--|------------------------------|-----------|--------|--------|--------|
| % Removal of CR dye by Using Tea Leaves at Different Temperatures | | | | | |
| Dye | Ci (M) (10 ⁵) | % REMOVAL | | | |
| | | 303K | 308K | 313K | 318K |
| CR dye | 0.1 | 79.96071 | 90.56 | 84.67 | 79.96 |
| | 0.3 | 88.14383 | 95.9 | 98.54 | 90.53 |
| | 0.5 | 99.45455 | 93.8 | 82 | 65.45 |
| | 0.7 | 71.20448 | 44.14 | 96.5 | 97.47 |
| | 0.01 | 77.37643 | 81.36 | 83.4 | 87.45 |
| | 0.003 | 93.83562 | 80.46 | 93.49 | 72.26 |
| % Removal of CR by Using Date Pits Powder at Different Temperatures | | | | | |
| Dye | Ci (M) (10 ⁵) | % REMOVAL | | | |
| | | 303K | 308K | 313K | 318K |
| CR dye | 0.1 | 93.90 | 85.46 | 96.86 | 97.24 |
| | 0.3 | 70.74 | 98.2 | 99.22 | 96.89 |
| | 0.5 | 92.181 | 74.18 | 96.545 | 96.72 |
| | 0.7 | 91.372 | 98.03 | 98.823 | 99.66 |
| | 0.01 | 85.741 | 96.38 | 92.96 | 96.95 |
| | 0.003 | 94.863 | 95.27 | 93.15 | 91.78 |
| % Removal of MGO dye by Using Corn Husk Powder at Different Temperatures | | | | | |
| Dye | Ci (M) (10 ⁵) | % REMOVAL | | | |
| | | 303K | 308K | 313K | 318K |
| MGO dye | 0.1 | 88.6 | 91.40 | 87.94 | 88.18 |
| | 3 | 92 | 94.10 | 93.11 | 95.45 |
| | 5 | 95 | 95.30 | 91.58 | 89.61 |
| | 7 | 91 | 91.44 | 91 | 90.43 |
| | 8 | 94 | 95.95 | 93 | 93.69 |
| | 9 | 90 | 90 | 92.07 | 99.25 |
| % Removal of MGO dye by Using Peach Seed Powder at Different Temperatures | | | | | |
| Dye | Ci (M) (10 ⁵) | % REMOVAL | | | |
| | | 303K | 308K | 313K | 318K |
| MGO Dye | 0.1 | 95.836 | 95.970 | 95.903 | 96.642 |
| | 3 | 98.522 | 92.366 | 98.365 | 93.082 |

| | | | | | |
|--|---|--------|--------|--------|--------|
| | 5 | 89.939 | 98.616 | 98.186 | 98.871 |
| | 7 | 95.074 | 91.269 | 90.597 | 91.045 |
| | 8 | 94.224 | 88.314 | 94.358 | 90.463 |
| | 9 | 95.202 | 91.844 | 96.450 | 94.531 |

TABLE: 4 LANGMUIR ISOTHERMS

| Langmuir parameters for used tea leaves powder | | | | | | |
|--|-------------|-----------|--------|----------------|---------------------|----------------|
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | 1/K Vm | 1/Vm | K _L | Vm x10 ⁵ | |
| 01 | 303 | 2.2228 | 94396 | 42467.158 | 1.059 | 0.005 |
| 02 | 308 | 1.6251 | 11680 | 7187.250 | 8.516 | 0.344 |
| 03 | 313 | -0.5367 | 12888 | 24013.415 | 7.759 | 0.738 |
| 04 | 318 | 0.9372 | 75764 | 80840.802 | 1.319 | 0.212 |
| Langmuir parameters for date pits powder | | | | | | |
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | 1/K Vm | 1/Vm | K _L | Vm x10 ⁵ | |
| 01 | 303 | 0.586 | 21313 | 36351.697 | 4.691 | 0.604 |
| 02 | 308 | 2.697 | 46629 | 17286.005 | 2.144 | 0.744 |
| 03 | 313 | 2.818 | 13955 | 4950.512 | 8.425 | 0.188 |
| 04 | 318 | 0.556 | 9277.2 | 16682.611 | 1.077 | 0.471 |
| Langmuir parameters for prunus persica seeds shell powder | | | | | | |
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | 1/K Vm | 1/Vm | K _L | Vm | |
| 01 | 303 | 0.483 | 0.006 | 0.01240 | 166.66 | 0.0466 |
| 02 | 308 | 0.151 | 0.0254 | 0.1674 | 39.370 | 0.7065 |
| 03 | 313 | 0.331 | 0.0234 | 0.070652 | 42.7350 | 0.7999 |
| 04 | 318 | 0.252 | 0.0294 | 0.11638 | 34.0136 | 0.5833 |
| Langmuir parameters for corn husk powder | | | | | | |
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | 1/K Vm | 1/Vm | K _L | Vm | |
| 01 | 303 | 0.238 | 4792 | 20100.677 | 2.086 | 0.004 |
| 02 | 308 | 0.168 | 0.0555 | 0.330 | 18.018 | 0.003 |
| 03 | 313 | 0.013 | 0.0012 | 0.092 | 8333.330 | 0.028 |

| | | | | | | |
|----|-----|-------|--------|-------|--------|-------|
| 04 | 318 | 0.127 | 0.0626 | 0.497 | 15.974 | 0.007 |
|----|-----|-------|--------|-------|--------|-------|

TABLE: 5 FREUNLICH ISOTHERMS

| Freundlich parameters for tea leaves powder | | | | | | |
|--|-------------|-----------|---------|---------------------------------|----------|----------------|
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | log k | 1/n | K _F x10 ⁴ | N | |
| 01 | 303 | -3.212 | 0.188 | 6.136 | 5.302 | 0.181 |
| 02 | 308 | -3.143 | 0.291 | 7.189 | 3.427 | 0.236 |
| 03 | 313 | -3.221 | 0.194 | 6.010 | 5.154 | 0.289 |
| 04 | 318 | -3.687 | 0.107 | 2.055 | 9.302 | 0.025 |
| Freundlich parameters for date pits powder | | | | | | |
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | log k | 1/n | K _F x10 ⁴ | N | |
| 01 | 303 | -3.2842 | 0.2823 | 5.197 | 3.542 | 0.445 |
| 02 | 308 | -4.7056 | 0.0155 | 0.198 | 64.516 | 0.003 |
| 03 | 313 | -4.4907 | 0.0836 | 0.323 | 11.961 | 0.055 |
| 04 | 318 | -2.9024 | 0.3074 | 1.251 | 3.253 | 0.443 |
| Freundlich parameters for prunus persica seeds shell powder | | | | | | |
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | log k | 1/n | K _F x10 ³ | N | |
| 01 | 303 | 0.049 | 0.9475\ | 1.121 | 1.055 | 0.707 |
| 02 | 308 | -2.315 | 0.460 | 4.835 | 2.172 | 0.436 |
| 03 | 313 | -2.814 | 0.391 | 1.533 | 2.556 | 0.805 |
| 04 | 318 | -2.385 | 0.466 | 4.114 | 2.141 | 0.359 |
| Freundlich parameters for corn husk powder | | | | | | |
| S. No. | Temperature | Intercept | Slope | Constant | Constant | R ² |
| | K | log k | 1/n | K _F | N | |
| 01 | 303 | 4.652 | 1.835 | 44946.926 | 0.544 | 0.889 |
| 02 | 308 | 2.604 | 1.415 | 401.883 | 0.706 | 0.799 |
| 03 | 313 | 3.411 | 1.570 | 2581.071 | 0.032 | 0.895 |
| 04 | 318 | -0.409 | 0.773 | 2.565 | 1.292 | 0.894 |

TABLE: 6 ADSORPTION KINETICS

| Pseudo second order kinetics | | | |
|-------------------------------------|-----------|--------|----------------|
| Adsorbents | Intercept | Slope | R ² |
| Date pits powder | 1E+06 | 2026.3 | 0.006 |
| Peach seeds powder | -87390 | 46005 | 0.712 |
| Grounded Tea leaves | -102615 | 9140.5 | 0.887 |
| Grounded Corn Husk | 17524 | -26456 | 0.904 |

TABLE: 7 THERMODYNAMIC PARAMETERS

| Samples | T (K) | ΔG° (KJmol ⁻¹) | ΔH° (KJmol ⁻¹) | ΔS° (KJmol ⁻¹) | Ln k | 1/T |
|-------------|-------|---|---|---|--------|-------------------------|
| Tea Leaves | 303 | -26845.520 | -1816.9 | 16.181 | 10.656 | 3.30x10 ⁻³ |
| | 308 | -22739.286 | | | 8.880 | 3.246 x10 ⁻³ |
| | 313 | -26247.573 | | | 10.086 | 3.194 x10 ⁻³ |
| | 318 | -29876.154 | | | 11.300 | 3.144 x10 ⁻³ |
| Date Pits | 303 | -26453.500 | 3318.4 | -0.9188 | 10.502 | 3.30x10 ⁻³ |
| | 308 | -24986.537 | | | 9.757 | 3.246 x10 ⁻³ |
| | 313 | -25542.153 | | | 9.815 | 3.194 x10 ⁻³ |
| | 318 | -25703.852 | | | 9.722 | 3.144 x10 ⁻³ |
| Corn Husk | 303 | -24960.939 | 52465 | -170.4 | 9.908 | 3.30x10 ⁻³ |
| | 308 | 2838.9656 | | | -1.108 | 3.246 x10 ⁻³ |
| | 313 | 6186.4274 | | | -2.382 | 3.194 x10 ⁻³ |
| | 318 | 1876.566 | | | -0.709 | 3.144 x10 ⁻³ |
| Peach Seeds | 303 | 1204.465 | -8486.3 | 25.048 | -4.390 | 3.30x10 ⁻³ |
| | 308 | 4576.937 | | | -1.787 | 3.246 x10 ⁻³ |
| | 313 | 6896.0183 | | | -2.649 | 3.194 x10 ⁻³ |
| | 318 | 5686.646 | | | -2.150 | 3.144 x10 ⁻³ |

FIGURES

OPTIMIZATION OF AMOUNT

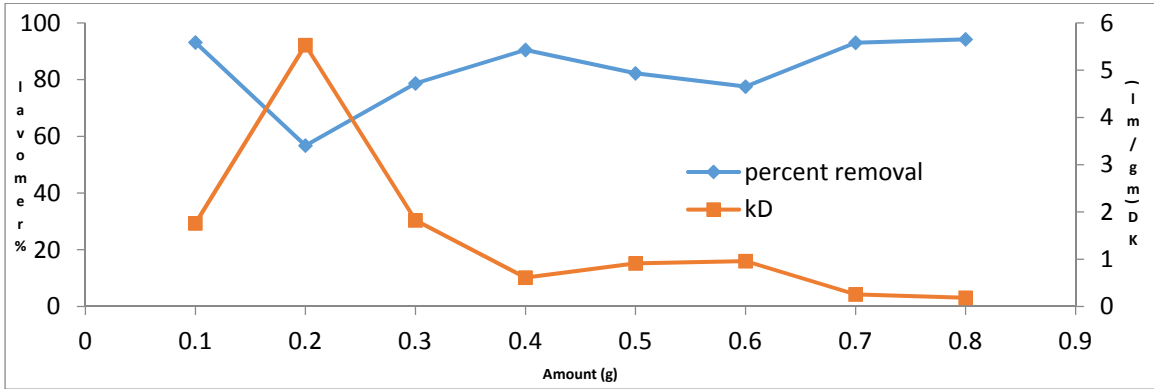


Figure 1: Optimization of amount for elimination of Congo red dye by using used tea leaves powder

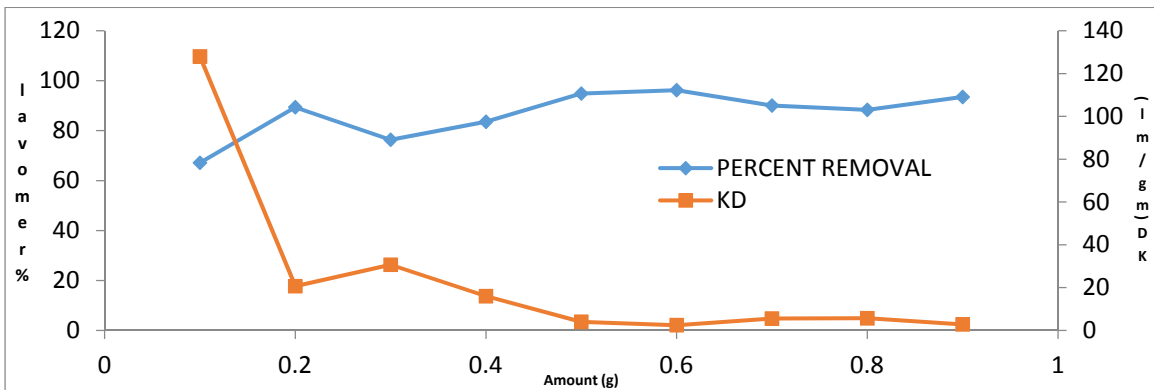


Figure 2: Optimization of amount for elimination of Congo red dye by using date pits powder

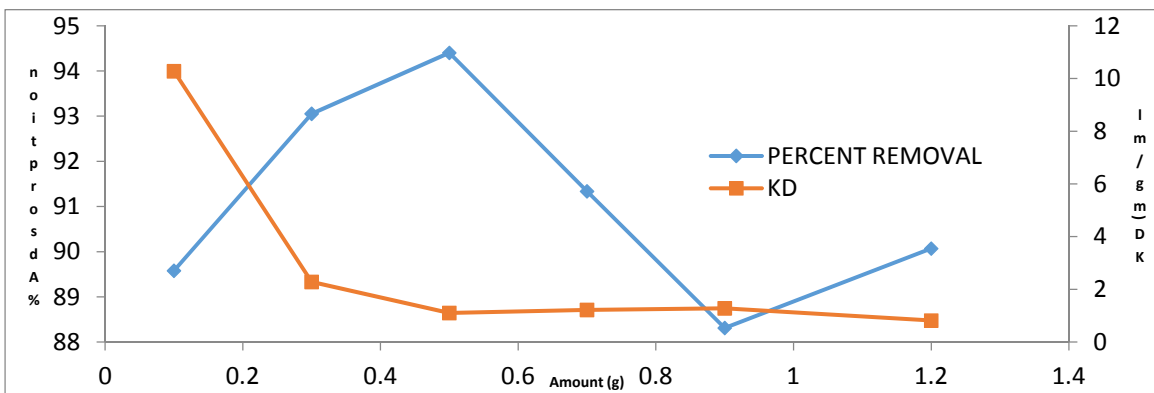


Figure 3: Optimization of amount for elimination of Malachite green oxalate dye by using Corn Husk powder

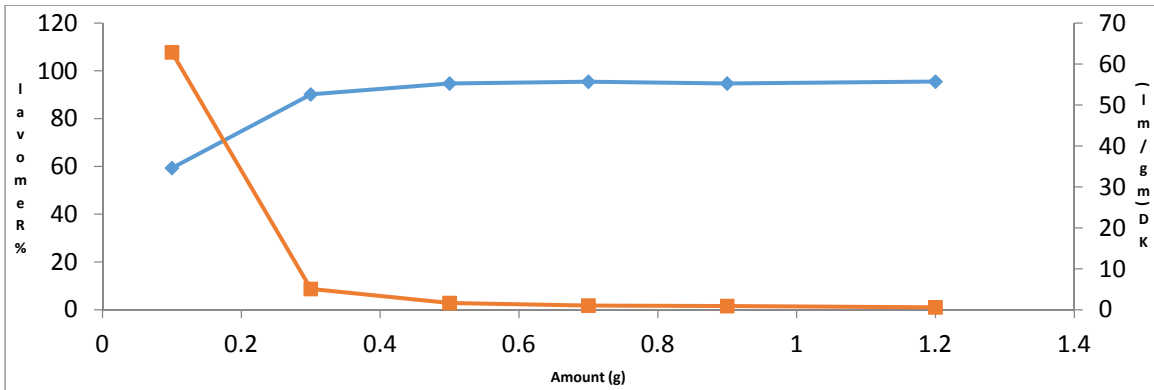


Figure 4: Optimization of amount for elimination of MGO dye by using Peach Seed powder

OPTIMIZATION OF TIME

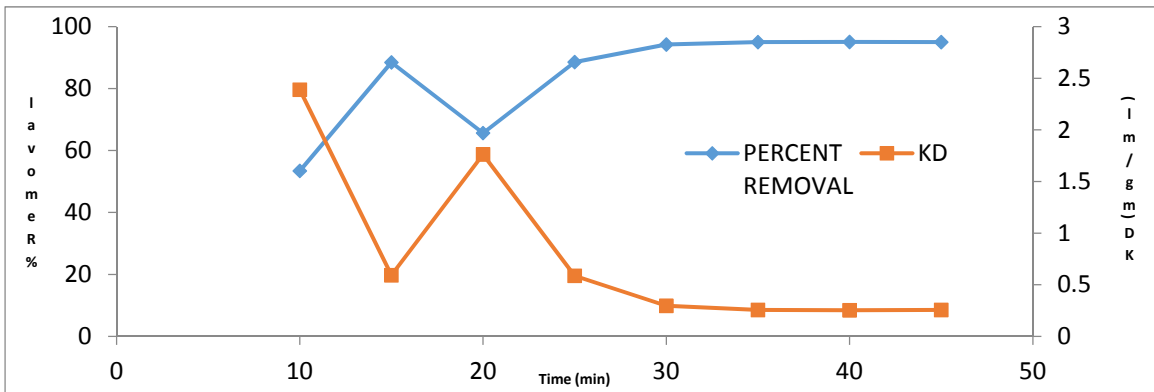


Figure 5: Optimization of time for removal of Congo red dye by using Tea leaves powder

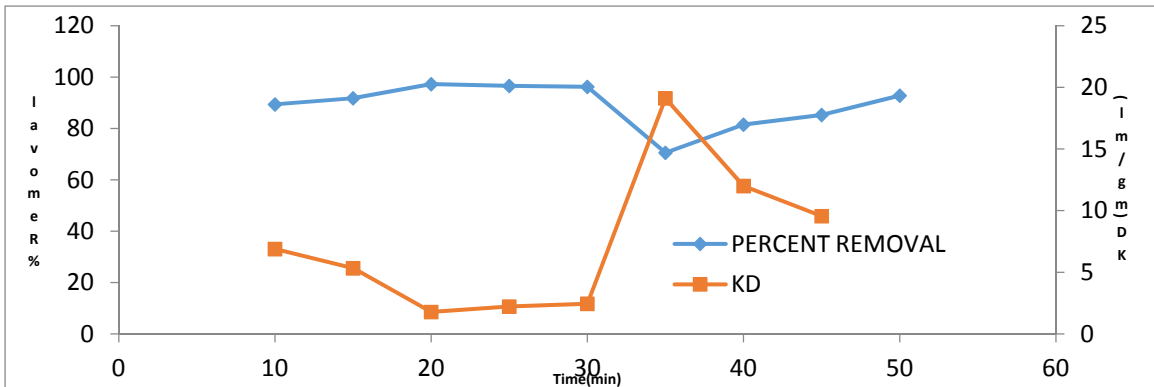


Figure 6: Optimization of time for elimination of Congo red dye by using Date pits powder

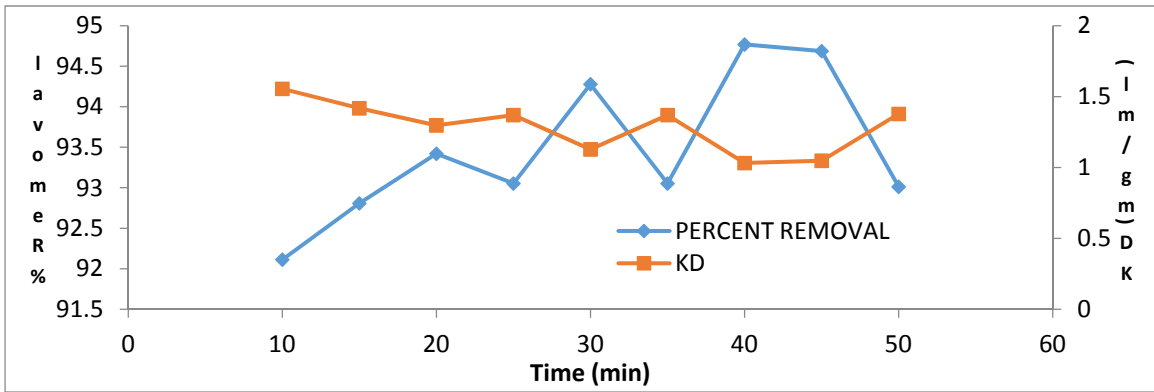


Figure 7: Optimization of time for elimination of Malachite green oxalate dye by using Corn husk powder

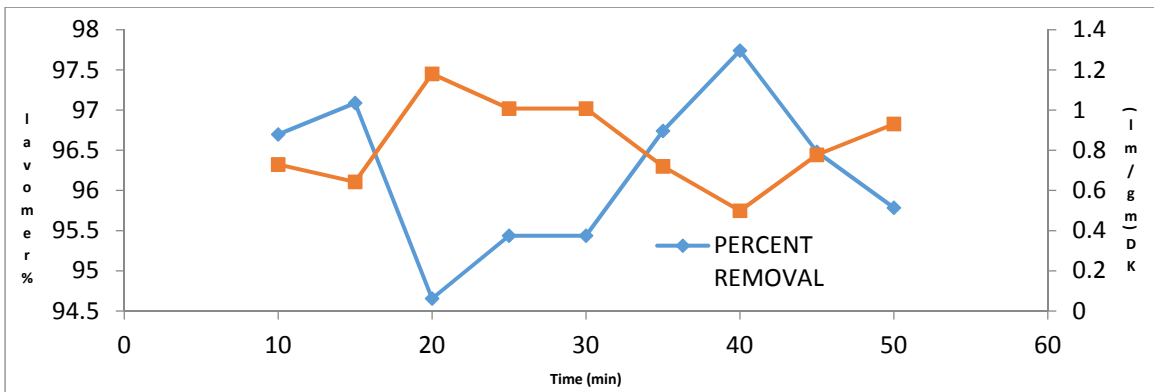


Figure 8: Optimization of time for elimination of Malachite green oxalate dye by using Peach seed powder

ADSORPTION KINETICS

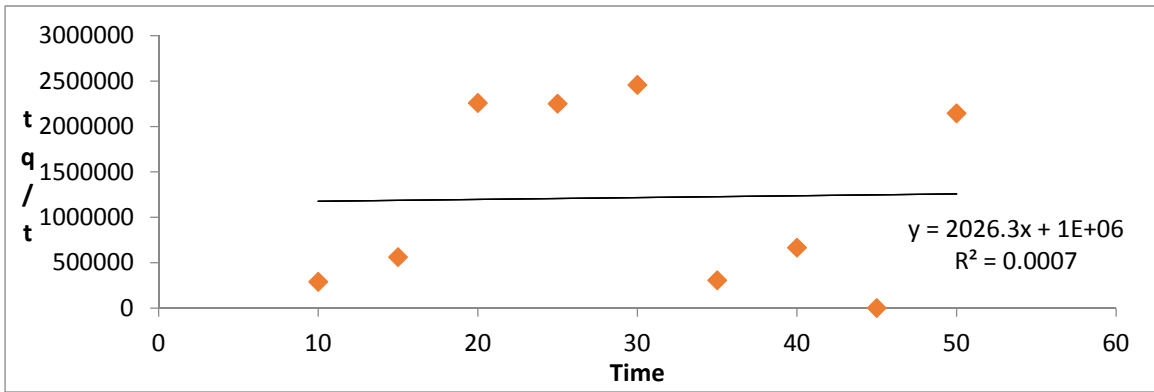


Figure 9: kinetics of date pits by Pseudo -second order

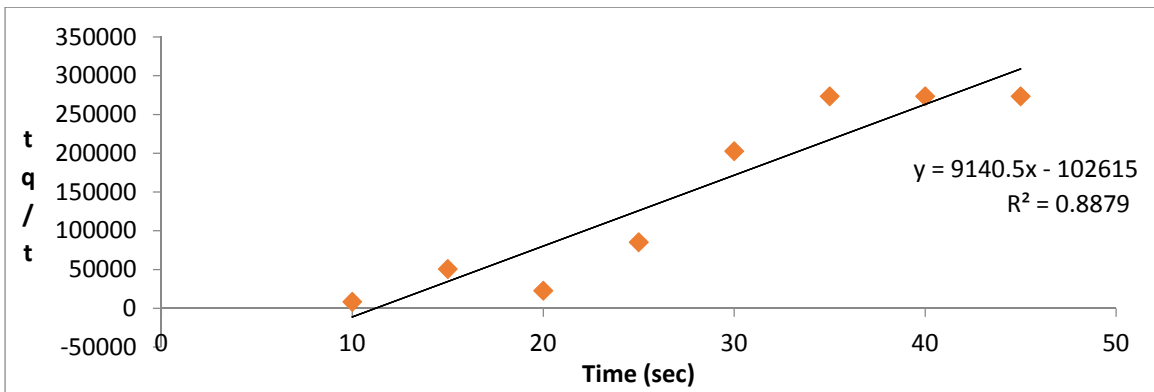


Figure 10: kinetics of tea leaves by Pseudo -second order

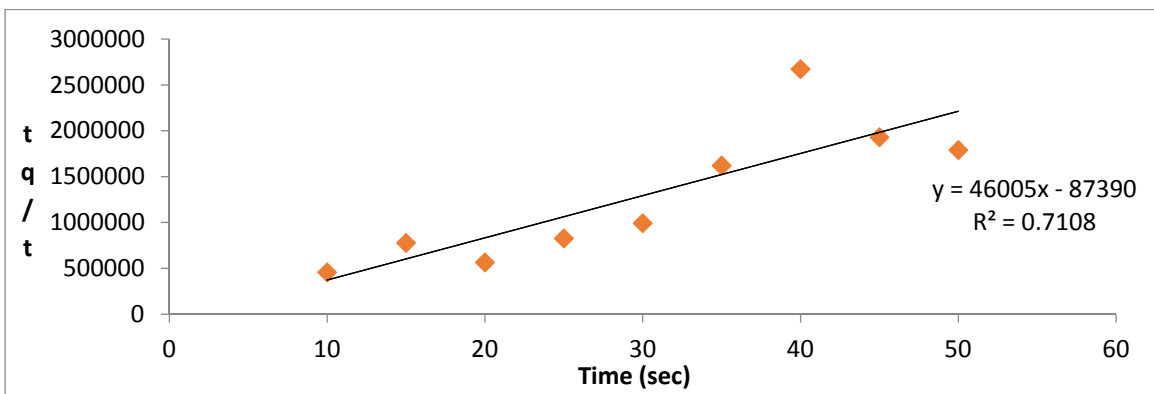


Figure 11: kinetics of peach seeds by Pseudo -second order

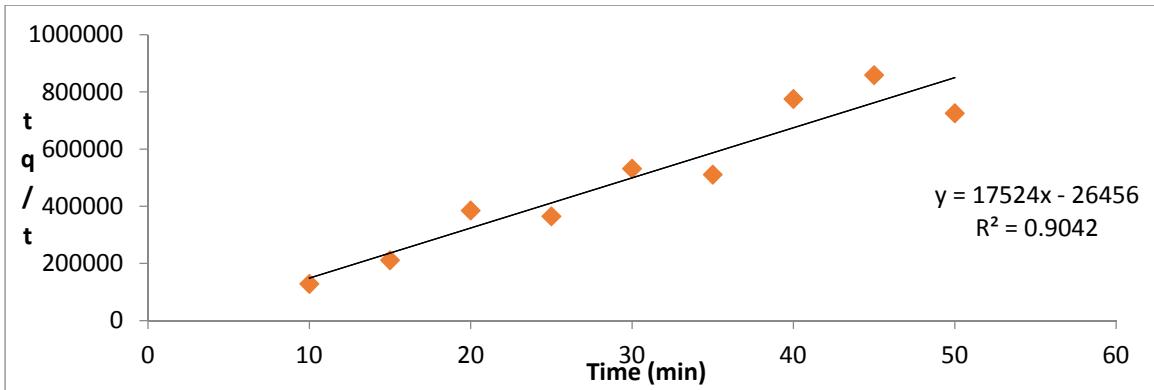


Figure 12: kinetics of corn husk by Pseudo -second order

Set 1: Tea waste, Set 2: corn husk, Set 3: peach seeds Set 4: date pits

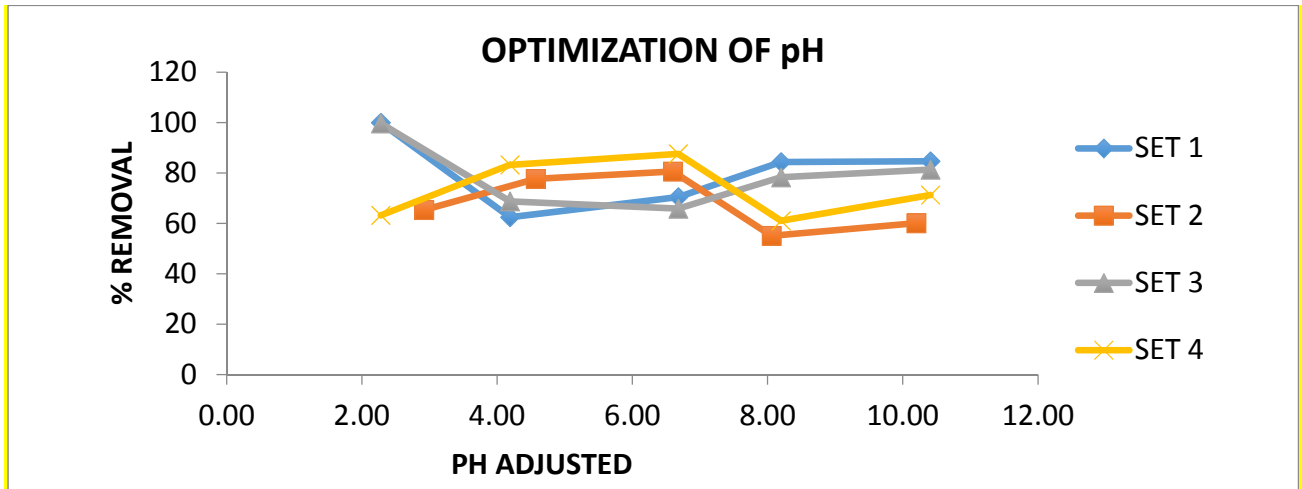


Figure: 13 OPTIMIZATION OF pH

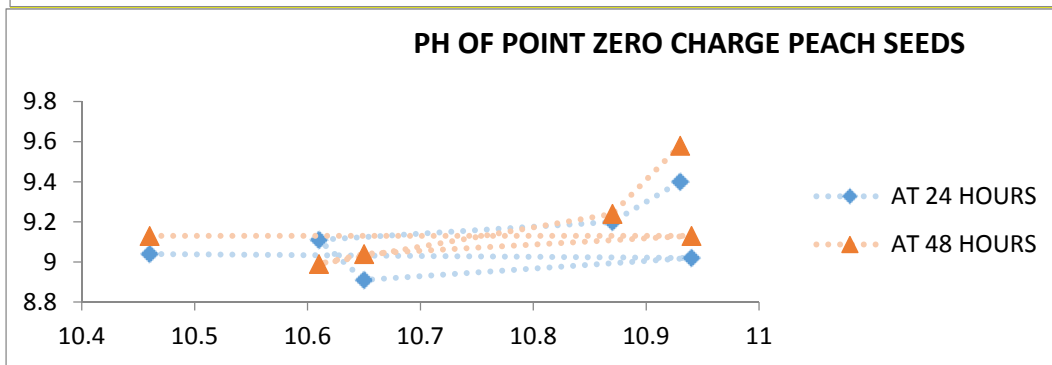
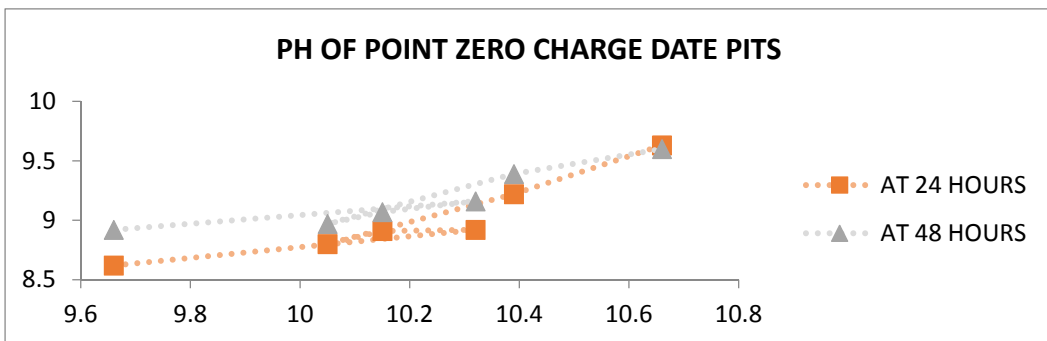
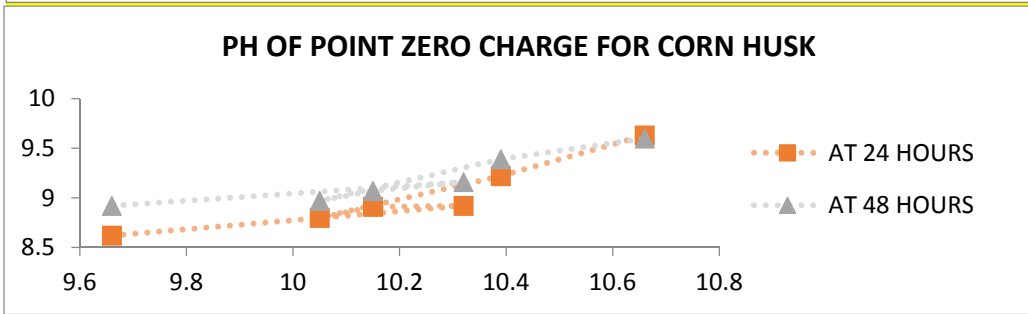
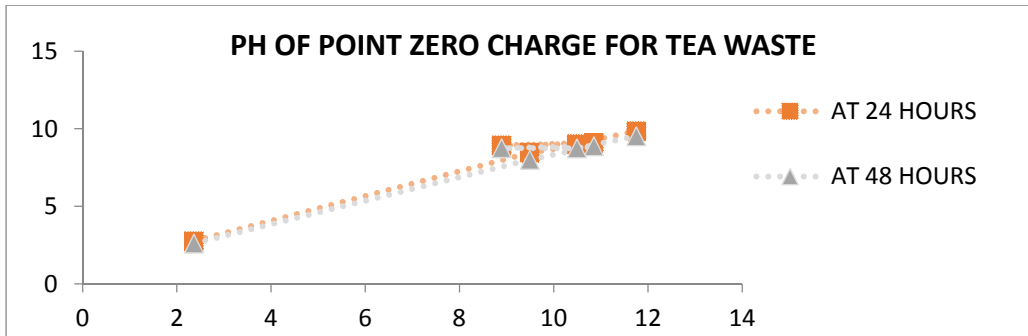


Figure: 14 OPTIMIZATION OF pH (pzc)

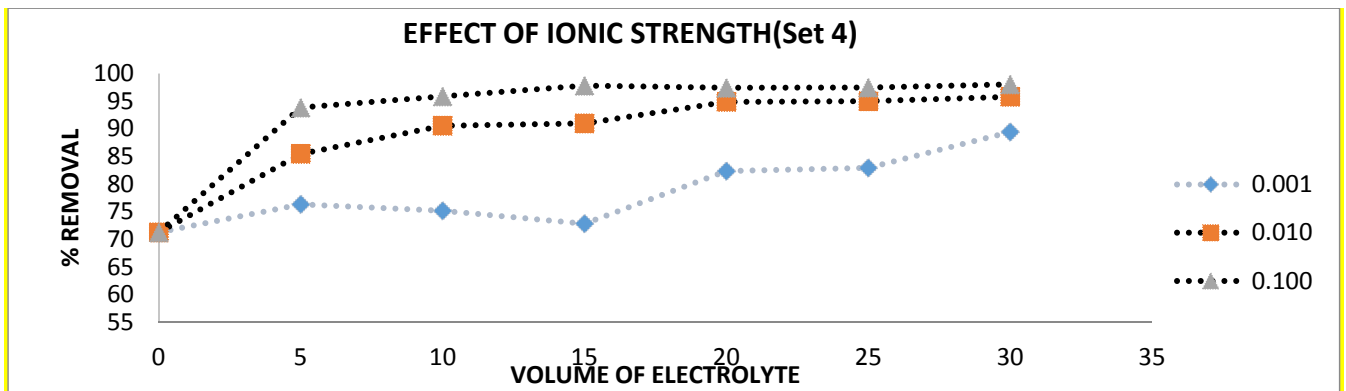
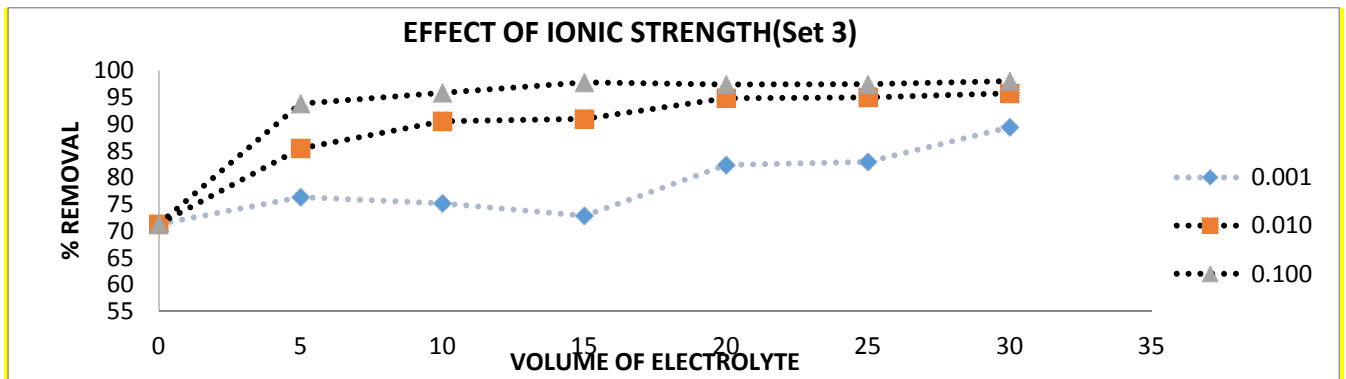
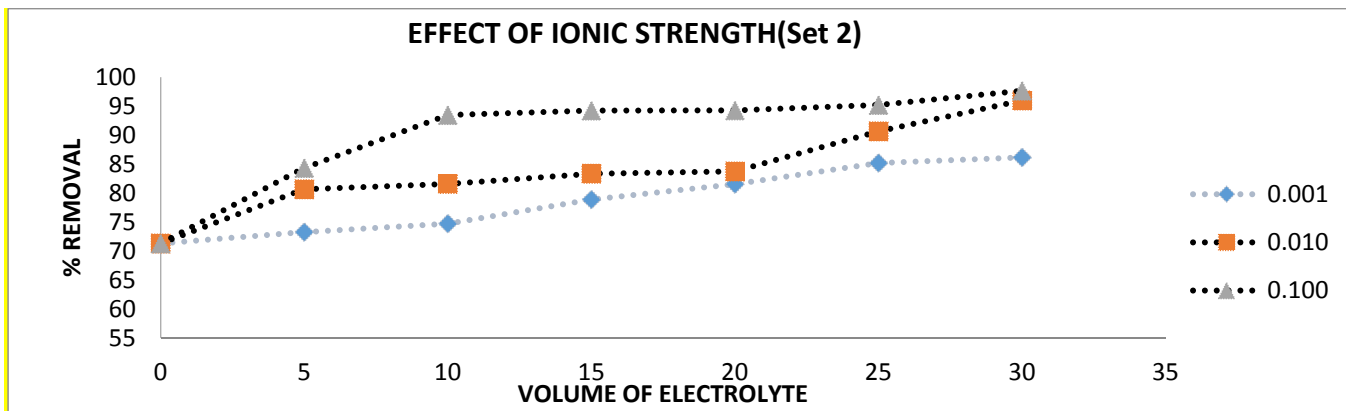
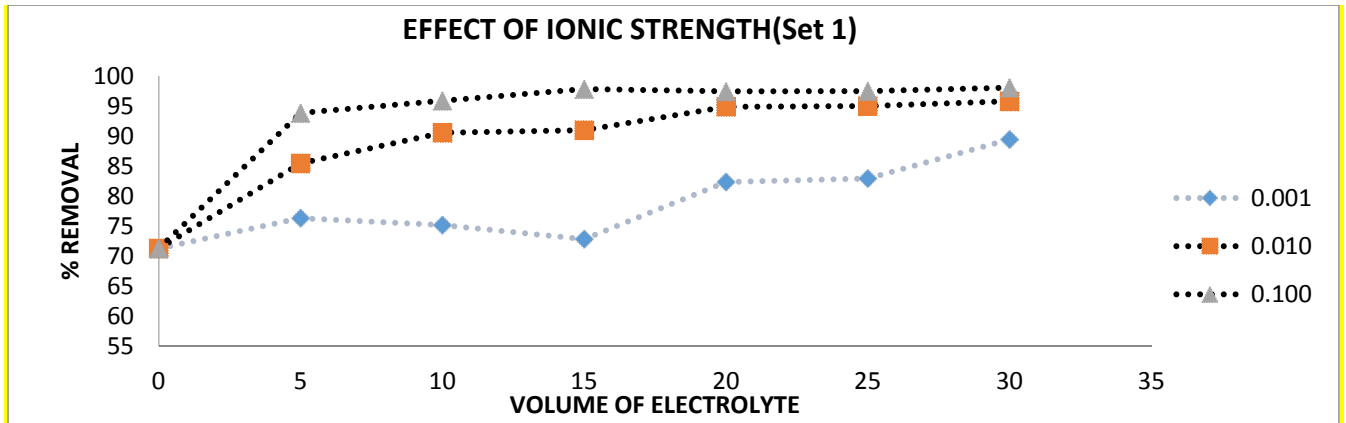
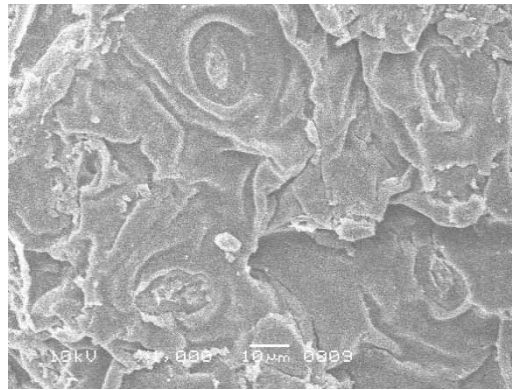
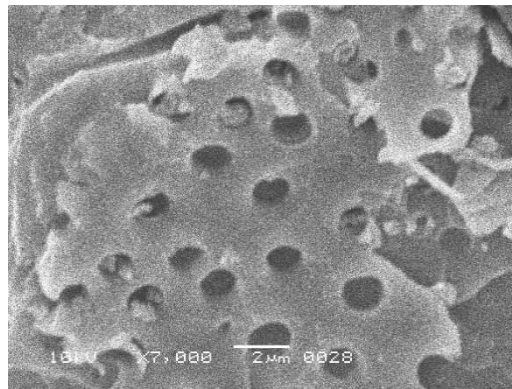


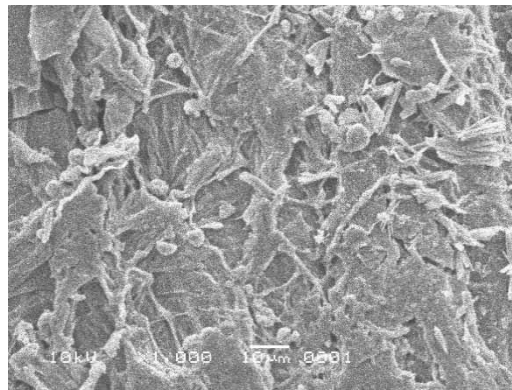
Figure: 15 OPTIMIZATION OF IONIC STRENGTH



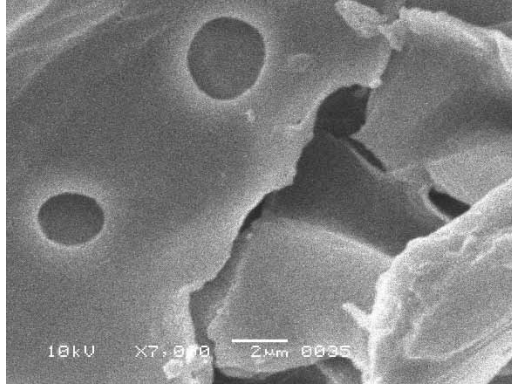
SEM images of tea leaves before adsorption



SEM images of tea leaves after adsorption



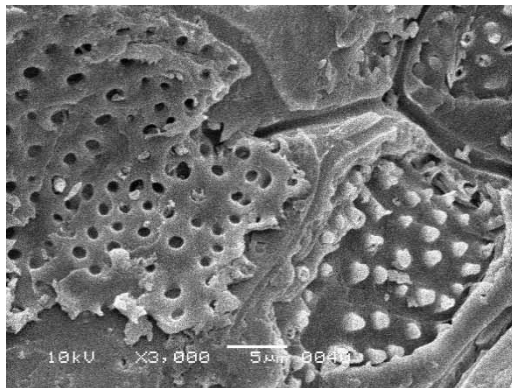
SEM images of corn husk before adsorption



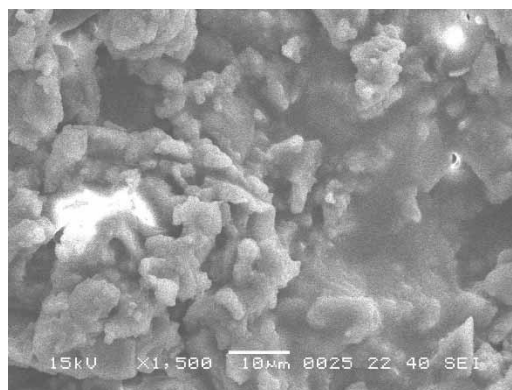
SEM images of corn husk after adsorption



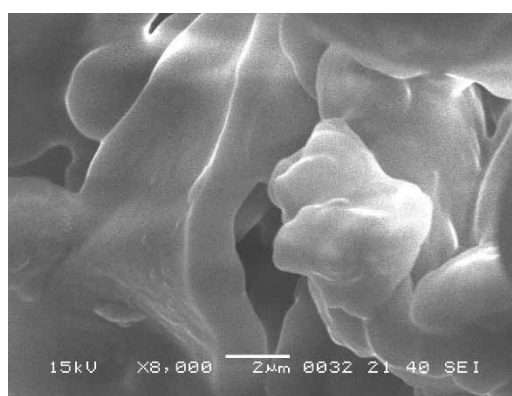
SEM image of peach seed before adsorption



SEM image of peach seed after adsorption



SEM image of Date pits before adsorption



SEM image of Date pits after adsorption

RESULTS AND DISCUSSION

Adsorption of carcinogenic dyes Congo Red (CR) was carried out by tea leaves powder and date pits powder. Adsorption of MGO dye was carried out by peach seeds powder and corn husk powder. Different experiments were performed in the adjusted circumstances of adsorbent's amount in table 1, adsorbents stay time in table 2 and adsorbents were analyzed at different temperatures in table 3. Concentrations of dyes before and after adsorption were recorded by ultraviolet visible spectrophotometer. The structure of natural adsorbents were analyzed by SEM technique.

Examination of effects of adsorption parameters on the adsorption

Effect of adsorbent's Amount

The optimum amount of adsorbent was taken as 0.4g for tea leaves in figure 1, 0.6g for date pits in figure 2, 0.5 g for corn husk in figure 3 and 0.5g for peach seeds powder in figure 4. By

Further increasing of amount of natural bio sorbents did not show any effective removal of dyes as shown in table 1.

Effect of p H

The zero point charge (Ppzc) of tea waste, corn husk, peach seeds and date pits were determined. Adsorption of cation is favored at $\text{pH} > 7$, while the adsorption of anion is favored at $\text{pH} < 7$. At $\text{pH} 2.0$ a significantly high-electrostatic attraction exists between the positively charged surface of the adsorbent and anionic dye. As the pH of the system increases, the number of negatively charged sites increases and the number of positively charged sites decreases. A negatively charged surface site on the adsorbent does not favor the adsorption of dye anions due to the electrostatic repulsion. Also, lower adsorption of dyes at alkaline pH is due to the presence of excess ions competing with the dye anions for the adsorption sites. Nevertheless, significant adsorption of anionic dye on the adsorbent still occurred above due to the fact that a chemical interaction between the dyes and tea waste, corn husk, peach seeds and date pits.

Effect of Ionic Strength

Different concentrations of KCl (0.01–0.05 M) were added to investigate the effect of ionic strength on adsorptive removal of dyes. The increase in ionic strength causes increase in the adsorption of congo red and malachite green oxalate. Salt addition increases the aggregation of dye molecules and decreases the solubility. An increase in aggregation promotes the adsorption of dyes molecules. Another possibility is that increase in ionic strength increases the positive charge of the adsorbent on the surface thus increases the electrostatic attraction between dyes and adsorbents. Thus increase in ionic strength was found to have an increase in adsorption of both dyes.

Effect of stay time

For tea leaves - congo red system, maximum adsorption was obtained at 35 minutes in figure 5, for date pits – congo red system, maximum adsorption capacity was obtained at 20 minutes in figure 6, for corn husk- malachite green oxalate system, maximum adsorption capacity was acquired at 30 minutes in figure 7 and for peach seeds – malachite green oxalate system, extreme adsorption capacity was achieved at 15 minutes, as shown in figure 8.

Adsorption Isotherms

Langmuir adsorption isotherm

This isotherm shows monolayer adsorption on a consistent surface. Monolayer adsorption must be merely defined by Langmuir adsorption isotherm. Well-known Langmuir equation is as follows:

$$C_e/X/m = 1/KV_m + C_e/V_m$$

Here, equilibrium concentration is C_e (mol/dm³), amount adsorbed at equilibrium is X/m (mol/g), intercept is V_m (mol/g) and slope is K (dm³/mol). Graph with the straight line was assimilated by plotting " $C_e/X/m$ " on y-axis versus " C_e " on x-axis. From the slopes " V_m " and " K " intercepts were studied. The adsorption of Congo Red (CR) and malachite green oxalate (MGO) were examined at different temperatures.

The results indicated that that in case of Tea leaves-Congo red dye system there were decreasing in the values of slope with the increase of temperature from 303K to 313K it proved the strong adsorbate-adsorbent contact at low temperatures. It also revealed that adsorption attraction of dye was dropped with the increased in temperature, therefore adsorption was auspicious at low temperatures. It also prophesied that strong adsorbate-adsorbent attraction occurred at lower temperatures.

The monolayer capacity (V_m), for congo red – tea leaves system formed onto the homogenous adsorbent surface. The value of K was positive presenting that they followed the Langmuir adsorption isotherm. The largest R^2 values of adsorbent-dye endorsed that adsorption happens according to Langmuir isotherm and monolayer forms onto the homogenous adsorbent surface as shown in figs. (9-12).

In the case of Date pits powder-Congo red dye system there was decrease in the values of the Langmuir constant with the increased in temperature from 303K to 318K which showed strong adsorbate-adsorbent interaction at low temperature. It also proved that attraction of dye reduced with rise in temperature therefore adsorption process was favorable at low temperatures.

Capability of monolayer (V_m), for Congo red – date pits system forms onto the homogenous adsorbent surface. The values of K were positive proved that which followed the Langmuir adsorption isotherm. The largest value of R^2 was 0.7446 obtained at 308K recommended that

strong adsorption occurred according to Langmuir adsorption isotherm and monolayer formed onto the homogenous adsorbent surface.

In Peach seeds powder- Malachite green oxalate dye system there were increased in the values of the Langmuir constant with the increased in temperature from 303K to 318K. It predicted that the strong adsorbate-adsorbent occurred at highest temperature. It also revealed that the adsorption of dye increased with the rise in temperature consequently adsorption was encouraged at high temperature.

The values of K were positive proved that they were followed the Langmuir adsorption isotherm. The largest values of R^2 were 0.7999, 0.7065 and 0.583 at temperature 313K, 308K and 318K respectively showed that the strong adsorption occurred conferring to Langmuir adsorption isotherm and monolayer was formed onto the homogenous adsorbent surface.

In the situation of Corn husk- Malachite green oxalate dye system, values of “K” increase with the increase in temperature from 303K to 318K. It oracles strong adsorbate-adsorbent interaction at higher temperatures. It also disclosed that adsorption of dye increased with increase in temperature so adsorption is encouraging at high temperature.

Monolayer capacity (V_m), for malachite green oxalate – corn husk system formed onto the homogenous adsorbent surface. The values of K were positive offering that they followed the Langmuir adsorption isotherm. The largest values of R^2 was 0.0274 assimilated at 313K confirming that strong adsorption occur according to Langmuir adsorption isotherm and monolayer formed onto the homogenous adsorbent surface.

The Freundlich adsorption isotherm

This isotherm is specified by the following equation:

$$\text{Log}X/m = \log K + 1/n \log C_e$$

Values of “K” and “n” were calculated from the intercepts and slopes of their relevant graphs and were written in Tables. Increase in values of constant (K) with the risen in temperature for

Congo red dye and malachite green oxalate dye showed that adsorption attraction of both dyes are favorable at higher temperatures [13].

In the case of Tea leaves- congo red system values of constant (K) decreased with the increase in temperature and showed that adsorption of dye was auspicious at lower temperature. With the rise in temperature decrease in the values of (K) occurred which showed there was high interaction with the adsorbent at lower temperature as shown in table (5). The values of “n” lies in between -1 to 10, which showed advantageous effect of the adsorption process. Values of R^2 proved that Freundlich isotherm, which showed formation of multilayer on the surface of adsorbent. The data fitted well in Freundlich isotherm with values of “n” which were 5.3022, 5.4270, 5.15, and 9.30 at temperatures 303K, 308K, 313K and 318 K respectively.

In the case of Date pits- Congo red system the values of (K) constant decreased with increased in temperature and showed that dye adsorption was auspicious at lower temperature. The decrease the values of K with the increase in temperature showed that there is high interaction with the adsorbent at lower temperature as presented in table (5). The values of R^2 were nearly about 0.999 showing that the adsorption followed Freundlich isotherm. The data fitted well in Freundlich isotherm with values of “n” 3.54 at 303K and 3.2530 at 318K.

In the case of Peach seeds- Malachite green oxalate system values of K constants were high at low temperatures which showed that adsorption of the dye was favorable at low temperature. Increase in the values of K with the decrease in temperature showed that there was high interaction with the adsorbent as showed in table (5). The values of R^2 were 0.707, 0.4364, 0.8059, 0.3589 at temperatures 303K, 308K, 313K and 318K respectively, showing that the adsorption followed Freundlich isotherm. Values of R^2 confirmed the Freundlich isotherm and showed the formation of multilayer on the surface of adsorbent. The data fitted well in Freundlich isotherm with the values of “n” 1.055, 2.1720, 2.55 and 2.1417 at temperatures 303K, 308K, 313K and 318 K respectively.

In case of Corn husk- Malachite green oxalate system values of (K) constants decreased with increased in temperatures which offered that adsorption of dye was favorable at low temperature. Decreased in the value of K with the increase in temperature showed that there is high interaction

with the adsorbent as presented in table (5). The values of R^2 were 0.8849, 0.7999, 0.8954 and 0.894 at temperatures 303K, 308K, 313K and 318 K respectively, which showed that the adsorption followed Freundlich isotherm. R^2 proved Freundlich isotherm and specified formation of multilayer on the surface of adsorbent. The data fitted well in Freundlich isotherm with the values of “n” 0.544, 0.70, 0.03 and 1.2923 at temperatures 303K, 308K, 313K and 318 K respectively.

Influence of thermodynamic parameter

Thermodynamic parameters of adsorption progression are used to accomplish the process of spontaneity. Change in Gibb's free energy measures the spontaneity. Its negative value proves the reaction is spontaneous.

ΔH^0 , ΔS^0 and ΔG^0 were premeditated by the following equations:

$$\Delta G^0 = \Delta H^0 - T\Delta S^0$$

$$\ln K_D = \Delta S^0/R - \Delta H^0/RT$$

$$\Delta G^0 = -RT \ln K_D$$

Here R, the gas constant, absolute temperature is T, equilibrium constant is K_D . ΔH^0 and ΔS^0 were obtained from slopes and intercepts of “ $\ln K_D$ ” versus $1/T$ [14].

Negative values of ΔG^0 confirms feasibility of method and spontaneity of adsorption with a maximum adsorption of dye. With the increase in temperature decrease in negative value of ΔG^0 specifies the adsorption progression of dye is auspicious at greater temperatures. Negative values of ΔG^0 and the positive value of ΔH^0 for tea leaves, date pits, corn husk proved the spontaneity of adsorption, whereas peach seeds shown the non-spontaneity of adsorption. Degree of randomness of a system is entropy. ΔS^0 positive describes structural alterations happen on the adsorbent, and the randomness occurs in the adsorption system. The positive value of ΔH^0 for date pits, corn husk proved the endothermic nature because there is a large increase of translational mobility on the surface and negative value of ΔH^0 for peach seeds, tea leaves shown the exothermic process of adsorption. The dye system confirmed (+) values of ΔS^0 describe the

randomness and negative values of ΔS^0 indicated some deviation in the adsorption system as shown in table 7.

Kinetics of adsorption

Linear graph of “ t/q_t ” on y-axis and “ t ” on x-axis for different concentrations of CR and MGO were plotted which correspond that sorption procedure followed pseudo-second order kinetic as displayed in Figure. q_e and q_t are the amount of the dye adsorbed on the adsorbent (mol/g) at equilibrium and t is time in minutes, k_2 is the adsorption of second order rate constant (mol/g.min). The correlation coefficients for the second order models are near to 0.999 shows the linearity with high degree of correlation coefficient Study of kinetics of adsorption offers the information regarding the rate of adsorption and practicability of adsorption procedure. The experimental results were pragmatic to examine kinetics by the models of pseudo-second order as shown in table 6 [15].

$$\ln(q_e - q_t) = \ln q_e - k_1 t$$

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{t}{q_e}$$

The values of R^2 for the MGO sorption on Peach seeds powder and Corn husk powder systems were obtained 0.7108 and 0.9042 and results of R^2 for CR sorption on Date pits powder and Tea leaves powder were analyzed to be 0.0007 and 0.8879. Results showed that system followed the pseudo second order kinetics, correlation coefficients for second order models are near 0.999 confirmed linearity with high degree of correlation coefficient.

Where k_{id} is intra-particle diffusion rate constant, which was obtained from slope of the linear plot of “ q_t ” verses “ $t_{1/2}$ ”. Intercept contributed the width of boundary layer i.e. greater intercept; the enhanced will be border layer effect. Positivity of slope expressed controlled adsorption process. Date pits powder, tea leaves powder, Peach seeds powder showed positive slope whereas corn husk exhibited negative slope as shown in table 6.

SEM interpretations of natural particles

Top characterization techniques is SEM. The scanning electron micrograph specifies that the particles are quite homogenous in nature and the size ranging from 50 - 120nm for natural bio sorbents. After the adsorption of tea leaves, date pits, corn husk and peach seed powder, the diameter of all the natural adsorbents were decreased because the dye coated onto their surfaces.

Conclusion

For the elimination of chemical toxins from water and waste water only adsorption is the familiar, effective and cheap method that yields high-quality results. The present research emphasizes on the removal of contaminants by using adsorption process with the collection natural adsorbents.

Different natural adsorbents like date pits, tea leaves, corn husk and peach seeds were used. The characterization of natural adsorbents characterization were analyzed by SEM. Malachite green oxalate dye adsorption was calculated and analyzed by using corn husk and peach seeds particles working as adsorbent under various conditions. Similarly adsorption of Congo red dye was considered by using waste tea leaves and date pits particles. The optimum circumstances for the adsorption of dyes adsorbents were presented. Investigational data presented adsorption followed the pseudo second order kinetics. Experimental data was form fitted well in Freundlich and Langmuir isotherms. After analyzing all the graphs and data it was concluded that Freundlich isotherm form fitted well approximately to all investigational adsorption data, and was particularly outstanding for extremely heterogeneous adsorbents. The negative value of ΔG° proved the spontaneity of adsorption of waste tea leaves powder, date pits powder and corn husk powder. The positive ΔG° value of Peach seeds powder confirmed non-spontaneity of the adsorption. The maximum removal of dyes by experimental results were found and it was concluded that this specific method could be employed on industrial scale for waste minimization. All natural adsorbents particles proposed a lot of auspicious benefits in the forthcoming era.

Treatment of dyes using fresh seeds powder was a highly economic and simple method than other methods meanwhile it has an excellent capability of eliminating color. Contaminated dyes which contaminate huge part of textile emission can be distorted into dull and non-toxic composites by this method. Hence, it is applicable for industrial pollutants for improving the worth of wastewater of fabric industries and numerous others. Furthermore effort for obtaining

other constraints of dye waste using the mentioned method can be conceded out to develop the adsorption proficiency.

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