

26 **Introduction**

27 Throughout the 20th century, oil and its derivatives became the main energy source, thus
28 leading to a global economic dependence [1]. Besides this, fossil fuels are a
29 major contributor to greenhouse gases emissions, leading to global climate changes. Biomass
30 can make a substantial contribution to supplying future energy demand in a sustainable way.
31 It is presently the largest global contributor of renewable energy [2]. Bioethanol is currently
32 the most widely used liquid biofuel in the world. Global ethanol production was about 13000
33 million gallons in 2007, and production has almost doubled over the past years, with a
34 production approaching 26000 million gallons for 2015 [3]. At present, bioethanol is
35 produced exclusively via 1st generation technologies, utilizing sugar and starch-rich
36 feedstocks, as no commercial size 2nd generation cellulosic ethanol facilities are presently in
37 operation [4]. Starch is a natural, cheap, available, renewable, and biodegradable
38 carbohydrate polymer produced by many plants as a source of stored energy. Bioethanol
39 production using starch rich materials, represents a cost-effective means for the production of
40 bio-alcohol comparing to the use of lignocelluloses [5]. Corn is the dominant material in the
41 starch to ethanol transformation industry worldwide [6]; however, wheat is the first available
42 material for the production of bioethanol in some regions [4]. Traditional conversion of starch
43 into alcohol requires a two-stage process: hydrolysis of starch by acid or amylolytic enzyme
44 and fermentation by anaerobic bacterium or yeast. Simultaneous saccharification and
45 fermentation with mixed cultures is an effective method for the direct fermentation of starch
46 offering the advantages of realization in one reactor and the glucose produced is rapidly
47 converted into ethanol [7]. However, in this system the ethanol yield decreases because starch
48 is consumed by the growth of amylolytic microorganisms. To increase the production of
49 ethanol, it is necessary to breed a microorganism by a genetic manipulation, which can
50 directly ferment starch into ethanol [8]. In the present study, two starch-rich products (wheat

51 and corn flours); were used as substrates for the production of ethanol. The raw starch
52 contained in the flours was pre-treated with crude amylase produced by the strain *B. subtilis*
53 TLO3, which optimal production conditions were previously investigated. Thereafter, the
54 released sugars in solution were fermented using the yeast *S. cerevisiae*. The results obtained
55 for the two flours were compared to determine the effect of amylase pre-treatment on each
56 substrate concerning starch hydrolysis and thus ethanol production.

57 **Methodology**

58 **1. Biological material**

59 Wheat (*Triticum durum*) and corn (*Zea mays*) flours were used as starch-rich substrates for
60 the production of bioethanol. The strain *Bacillus subtilis* TLO3 (accession number
61 KR262718) was isolated aseptically (15 cm depth) from rhizospheric soil of olive tree in the
62 region of Tlemcen (Algeria) and selected after a screening program from different sources
63 based on amylase production and physiological features (data not shown). The strain *S.*
64 *cerevisiae* S288C was obtained from a commercial source.

65 **2. Amylase production optimization**

66 Medium composition and production conditions were optimized to obtain the best
67 combination for optimal amylase production by the strain *B. subtilis* TLO3. The optimization
68 was done using the OVAT (One-Variable-at-Time) method and amylase activity was
69 analysed by estimating the released reducing ends of sugar according to the dinitrosalicylic
70 acid (DNS) method of Miller [9]. The sample to be assayed was mixed with starch 1%
71 buffered in sodium phosphate pH 6.8 (v/v); then the mixture was incubated for 30 min at
72 50°C. The reaction was stopped by adding the same volume of DNS reagent and boiled for
73 10 min at 100°C. The absorbance was read using a spectrophotometer at 540nm.
74 The experiments were realized using basal media containing 5g potato starch and 2g yeast
75 extract per 1000 ml distilled water (w/v), with pH 7 and shaking at 150 rpm. The production

media were sterilized by autoclaving at 121°C for 20min. The flasks were then cooled and inoculated with the 4% (v/v) *B. subtilis* TLO3 culture seed ($DO_{600} = 0.05$). The following parameters were tested: secondary carbon sources (glucose, cellobiose, sucrose, xylose, galactose, lactose, cellulose, tween 20, tween 80, glycerol (0,5%)); nitrogen sources (peptone, casein, yeast extract, urea, gelatine (0,25%), sodium nitrate and sodium nitrite (0,5%)); NaCl concentration (2,5, 5, 10, 15, 20, 25% (w/v)); pH (5,6,7,8,9,10); Temperature (28°C, 37°C, 50°C, 60°C and 80°C); Inoculum size (0,5, 1, 2, 3, 4, 5% (v/v)) and incubation time (24, 48, 72 hours).

3. Amylase production

Two 500 ml flasks containing 120 ml amylase production optimized medium were prepared. The strain *B. subtilis* TLO3 was cultivated on nutrient broth for 24h at 50°C. Three per cent of the culture (v/v) was inoculated to the amylase production media. After 24h of incubation at 50°C under orbital shaking 150 rpm, the media were centrifuged at 10000 rpm during 10 min at 4°C and the supernatants were used as crude amylase for the saccharification of the flours.

4. Wheat and corn flours saccharification

Ten grams of each flour was added to the crude supernatant then incubated under orbital shaking 150rpm at 45°C for 4h for wheat flour, and at 35°C for 24h for corn flour, in accordance with time and temperature of saccharification necessary for each starch [10, 11]. Samples were taken every hour and centrifuged at 10000 rpm for 10min to determine the amount of reducing sugars released. Media were finally centrifuged at 10000 rpm for 10 min at 4°C; then the supernatants autoclaved at 121°C for 20 min.

5. Reducing sugars fermentation using *Saccharomyces cerevisiae*

The strain *S. cerevisiae* S288C was cultivated on a Peptone-yeast-glucose PYG medium containing 1.25g peptone; 1.25g yeast extract and 3g glucose per 1000ml of distilled water (w/v); for 48h at 30°C. Each saccharification medium was inoculated with 5% yeast

101 culture(v/v) ($DO_{600}=0.05$). The media were then incubated at 30°C for 24h and samples were
102 taken each hour for the monitoring of reducing sugar and ethanol concentrations.

103 **6. Determination of reducing sugars and ethanol production**

104 The amount of reducing sugars was measured before and after flours saccharification and
105 throughout the fermentation process using the DNS method [9].Concerning the ethanol
106 production, it was determined by the colorimetric method described bySumbhateet al.[12]. A
107 mixture containing 0.5ml sample to be assayed, was mixed with 0.5ml sodium dichromate
108 reagent; 0.5ml acetate buffer pH 4.3 and 2.5ml sulphuric acid 1N. The solution was then
109 vortexed for 1min then incubated at room temperature for 120min. The absorbance was read
110 at 578nm using a spectrophotometer and a standard curve was plotted using different ethanol
111 concentrations.

112 **Results and discussion**

113 **1. Amylase production optimization**

114 The highest amylase production (367 ± 6 U/ml) was obtained using 0.5% starch as essential
115 carbon source, 0.5% xylose as secondary carbon source, 0.25% urea as nitrogen source, 2.5%
116 NaCl and 3% inoculum size. The production was at its optimumat initial pH 7, temperature
117 50°C and 24 h incubation period at 150 rpm shaking.

118 Many Firmicutes bacteria are able to utilize xylose as carbon source (Gu et al., 2010). Xylose
119 may be implied in ribose synthesis, an important sugar in nucleic acid formation. Indeed,
120 Parket al.[13]reported the isolation of transketolase deficient *B. subtilis* strain, which was
121 able to produce D-ribose from xylose. Nahas and Waldemarin[14] showed that xylose was
122 among the best supplementary carbon sources for highest amylase production using the fungi
123 *Aspergillusochraceus*.

124 Among organic and inorganic nitrogen sources employed, urea showed the highest amylase
125 activity, followed by sodium nitrate. This shows that this strain has no preference between

126 inorganic and organic nitrogen source for amylase production. Nagarajan *et al.*, [15] reported
127 maximum amylase production by *B.subtilis* strain using urea as nitrogen source.
128 The high production yield noted at high temperature is an asset in industrial enzyme
129 production because it influences both bacterial growth and amylase production[16]. Many
130 studies reported optimum amylase production in this temperature range using *Bacillus* strains
131 [17, 18, 19].
132 Also, maximum amylase production in short time(24h), represent promising results for
133 application at large scale allowing considerable energy savings. Similar works reported
134 maximum amylase activity after 24h using *Bacillus* strains [20, 21]. Optimization results are
135 presented in Table 1.

136 **2. Wheat and corn flours amylase pre-treatment**

137 Flours starch saccharification was performed using crude amylase produced by *B. subtilis*
138 TLO3 (Figure 1, Figure 2). A good yield of released reducing sugars was noted for both
139 flours. Thus, percentages of 70% and 91% of reducing sugars were obtained during the
140 saccharification of wheat and corn flours, respectively; proving the efficiency of starch
141 saccharification of the crude amylase produced by *B. subtilis* TLO3. Several studies reported
142 raw starch saccharification for bioethanol production using amylase produced by *Bacillus*
143 *spp.* strains[22, 23, 24, 25].

144 **3. Fermentation of reducing sugars and ethanol production**

145 The monitoring during 24h of reducing sugars fermented and ethanol produced is shown in
146 Figure 3 and Figure 4. The choice of an incubation time of 24h for the fermentation was
147 motivated by the advantage of production of ethanol in a short time which allows doing
148 considerable energy savings. The reducing sugars concentration at the beginning of the
149 fermentation was 100 µg/ml and 165 µg/ml, for wheat and corn flours, respectively. This
150 difference could be due to the starch content of corn 79% [26], which is superior to that of

151 wheat 62% [27]. The presence of resistant starch inaccessible to amylase enzymes up to 13%
152 for wheat flour and 8.1% for corn flour [28], can also explain that difference. The monitoring
153 of reducing sugars concentration during the fermentation showed a slight increase in the 3
154 first hours, which can be explained by a secretion of amylase by the yeast. Indeed, the strain *S.*
155 *cerevisiae* S288c possesses α -glucosidase MAL32 expressed in early log phase [29]. This
156 was followed by a continuous decrease reaching 42% and 79% less for wheat flour and maize,
157 respectively, comparing to initial concentrations. This decrease indicates clearly that the yeast
158 transformed the reducing sugars obtained after the saccharification of the flours
159 starch. Concerning ethanol production, the monitoring showed a production yield of 0.92 g/l
160 (2%) for the wheat flour and 1.1 g/l (2.4%) for the corn flour after 24h. For the wheat flour
161 the production was steady during the 4 first hours, and then a continuous increase was noticed
162 from the fifth hour. For the corn flour, after an increase during the 3 first hours, the amount of
163 ethanol declined during 3 hours, then resumed the increase in a continuous manner until 24h.
164 This decrease could be due to a contamination by an acetic acid bacteria, which could
165 ferment ethanol and transform it to acetic acid by an oxydo-reduction reaction [30, 31, 32],
166 which represents a limiting factor in bioethanol production process. The best ethanol yield
167 was obtained using corn flour because of the higher starch content, and thus fermentable
168 sugars. Evaluative studies concerning starch for ethanol yield optimization described five
169 criteria that influence the functional properties of starch : amylose/ amylopectin content [33,
170 34, 35, 36, 37], the morphology of starch granule [38], the fine structure of amylopectin [39,
171 40, 41], thermal properties [34, 36] and pasting properties [36].

172 **Conclusion:**

173 Bioethanol production using starch rich substrates remains, to the present, the most cost-
174 effective means for bio-alcohol production; due to ease of saccharification comparing to
175 lignocelluloses. Amylase production optimization has indicated that *B.subtilis* TLO3 is a

176 promising candidate for starch transformation industry due to high amylase activity,
 177 production at high temperature and reduced time. Raw corn and wheat starches were pre-
 178 treated with crude amylase produced using the obtained parameters combination and high
 179 saccharification yields were obtained. Also good ethanol production was achieved, after
 180 fermentation of the released reducing sugars by the yeast *S. cerevisiae* S288C.
 181 Corn flour showed the best saccharification yield and ethanol production, confirming that it
 182 is, so far, the best starch substrate for ethanol production. For further improvement, statistical
 183 design optimization of bioethanol production conditions is envisaged, with the aim to achieve
 184 a successful scale-up to industrial level production.

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Table 1 : Results of amylase production optimization

Secondary carbon source	Amylase activity (U/ml) (mean ± SD)
Glucose	182.5 ± 3
Galactose	254.44 ± 7
Xylose	347.22 ± 1
Cellobiose	231.66 ± 1
Saccharose	118.88 ± 2
Lactose	297.22 ± 8
Maltose	244.16 ± 6
Cellulose	81.66 ± 5

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Glycerol	159,72 ± 1
Tween 20	133,33 ± 7
Tween 80	117,5 ± 5
Nitrogen sources	Amylase activity (U/ml)
Peptone	86,6666667 ± 2
Yeast ext	126,6666667 ± 5
Casein	134,1666667 ± 7
Urea	165,2777778 ± 7
Gelatin	141,6666667 ± 6
NaNo2	61,1111111 ± 3
NaNo3	153,3333333 ± 5
NaCl (%)	Amylase activity (U/ml)
0	108,6111111 ± 1
2,5	151,9444444 ± 5
5	126,6666667 ± 10
10	94,4444444 ± 5
15	83,3333333 ± 3
20	63,8888889 ± 5
25	55 ± 2
pH	Amylase activity (U/ml)
5	109,7222222 ± 5
6	112,5 ± 7
7	153,8888889 ± 8
8	131,3888889 ± 8
9	108,3333333 ± 5
10	100,5555556 ± 2
Temperature	Amylase activity (U/ml)
28	93,8888889 ± 1
37	164,7222222 ± 4
50	167,2222222 ± 8
60	194,4444444 ± 5
80	45,2777778 ± 3
Inoculum size (%)	Amylase activity (U/ml)
0,5	115 ± 3
1	101,3888889 ± 3
2	107,5 ± 5
3	113,3333333 ± 7
4	108,6111111 ± 6
5	103,8888889 ± 1
Incubation time (h)	Amylase activity (U/ml)
24	108,6111111 ± 1
48	95,2777778 ± 5
72	85,8333333 ± 3

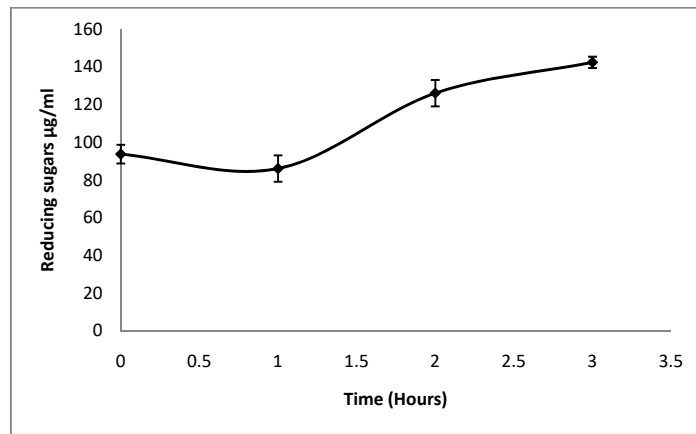


Figure 1.Reducing sugars released during the saccharification of wheat flour.

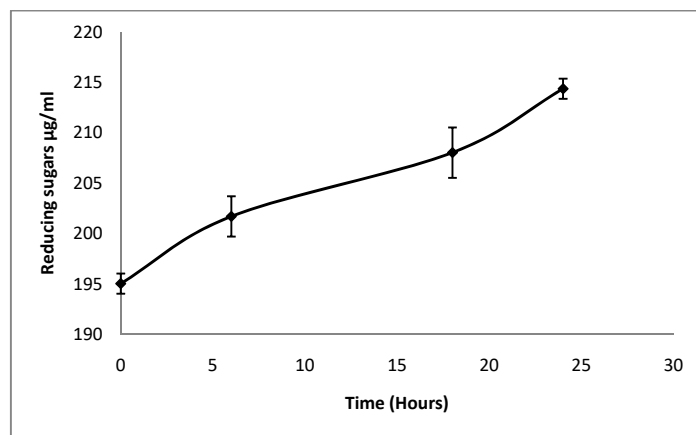


Figure 2. Reducing sugars released during the saccharification of corn flour.

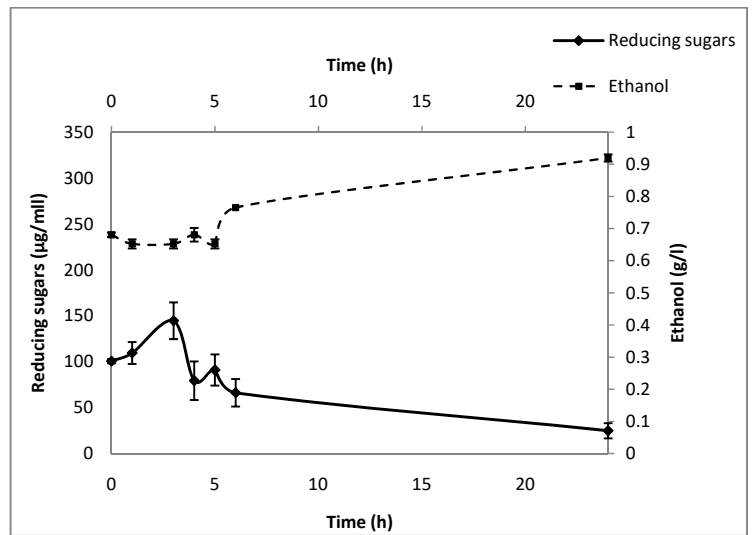


Figure 3. Amounts of ethanol produced and reducing sugars fermented during the fermentation of wheat flour using *Saccharomyces cerevisiae*.

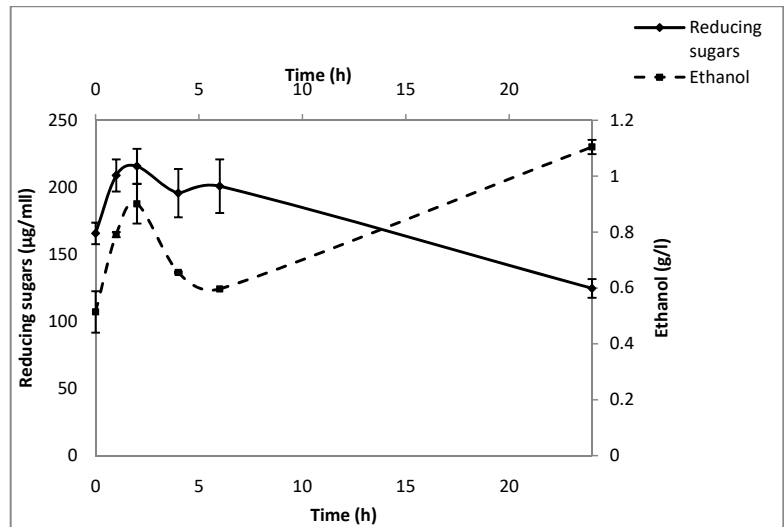


Figure 4. Amounts of ethanol produced and reducing sugars fermented during the fermentation of corn flour using *Saccharomyces cerevisiae*.