1	Original Research Article
2	Synthesis and Characterization of Pentaerythritol Diacrylate
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5	Abstract
6	Pentaerythritol diacrylate (PEDA) is synthesized by the esterification of pentaerythritol (PER) with
7	acrylic acid (AA) using p-toluenesulfonic acid (PTSA) supported on silica as a catalyst. Fourier
8	transform infrared spectrometer (FT-IR), and carbon nuclear magnetic resonance spectroscopy
9	(¹³ C-NMR) were used to characterize the product of PEDA purified by utilizing column chromatography.
10	The effects of various operating conditions such as the catalyst concentration(w_{cat}), the reactants mole
11	ratios (N_{AA}/N_{PER}), the reaction temperature (T) and time (t) on the yield of PEDA are investigated. The
12	results show that the yield of PEDA increases <mark>sharply with increase in <i>w</i>_{cat} until <i>w</i>_{cat} is 2.0 wt% and then</mark>
13	increases gently. The highest yield (64.5%) is obtained when the operation conditions are as follows:
14	w _{cat} =2.0 wt%, <i>N</i> _{AA} / <i>N</i> _{PER} =2.7, <i>T</i> =403 K and <i>t</i> =240 min.
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16	KEYWORDS: Pentaerythritol diacrylate, Pentaerythritol, Acrylic acid, PTSA-Silica catalyst,
17	Esterification
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19	1. Introduction
20	Pentaerythritol diacrylate (PEDA) is an important intermediate, and can be used to synthesize
21	some special purpose copolymers, such as the poly (PEDAS-co-TPTM) monolithic column ^[1] , the
22	waterborne polyurethane-acrylate (WPUA) ^[2] , and the acrylate chemical grouting materials ^[3] , which
23	can be applied in proteome analysis, UV-curing resins, and concrete construction works, respectively.
24	Additionally, PEDA is widely used as photoinitiator in the UV-curing field ^[4,5,6] . Especially, because it
25	contains two hydroxyl groups, PEDA can be incorporated in reactive hot melt polyurethane adhesives
26	(PURs) by replacing a portion of the polyols ^[7,8] . Meanwhile, as a dihydroxy-terminated acrylic monomer,
27	PEDA can increase the initial bond strength of PURs, to enhance the green strength of PURs ^[9-12] .
28	PEDA can be synthesized by esterification from pentaerythritol (PER) with acrylic acid (AA)
29	catalyzed by p-toluenesulfonic acid (PTSA) ^[3,7] . However, it is very difficult to separate PTSA from
30	PEDA products, which will reduce the product purity of PEDA. So, it is necessary to develop a new
31	catalyst which can be easily separated from the reaction system. The supported catalyst can be easily
32	removed by filtration ^[13-15] .
33	In this work, a supported catalyst (PTSA-Silica) was prepared by loading PTSA on silica gel, and
34	PEDA is synthesized by direct esterification using PTSA-Silica as a catalyst. The effects of various
35	reaction variables on the esterification conversion are investigated, including the reaction temperature
36	(<i>T</i>) and time (<i>t</i>), the mole ratio of acrylic acid to pentaerythritol (N_{AA}/N_{PER}) and the amount of catalyst
37	$(w_{cat}, defined as the mass percentage of the catalyst to the total reactants). The product of PEDA$
38	purified by chromatography and distillation in the sequence is characterized by infrared spectroscopy

39 (FT-IR), and ¹³C nuclear magnetic resonance spectroscopy (C-NMR).

4041 2. Materials and methods

42 **2.1. Reagents**

Pentaerythritol is purchased from Shanghai Titan technology co. LTD. Acrylic acid, sodium chloride, sodium hydroxide and anhydrous copper sulfate are obtained from Shanghai Chemical Co., Ltd. Hydroquinone, anhydrous copper sulfate, toluene, sodium chloride, sodium hydroxide and p-toluenesulfonic acid are bought from Shanghai Macklin Biochemical Co., Ltd. All the chemicals are analytical grade. The silica gel was obtained from Tsingdao Shuoyuan Chemical Co., Ltd. (Tsingdao, China), with a particle diameter of 0.20 ±0.02 mm, and its detailed physical parameters are shown in Table 1^[16].

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 Table 1. Physical Parameters of Silica Gel.

Parameters	Value
BET surface area, m^2/g	254.7
Volume of pores, cm^3/g	0.68
Pore diameter, Å	97
Apparent density, g/cm ³	1.02

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52 2.2. Preparation of the PTSA-Silica catalyst

The procedure for preparing the PTSA-Silica catalyst is similar to the literature^[17] and is briefly described as follows: To a solution of 0.04 mol PTSA·H₂O + 40 mL H₂O in a 100-mL beaker containing a stir bar was added 20 g of silica gel, and the mixture was stirred for 15 min and then gently heated on a hot plate, with intermittent swirling, until a free-flowing white solid was obtained. The catalyst was further dried by placing the beaker in an oven maintained at 120 °C for at least 48 h before use.

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59 2.3. Synthesis of PEDA

The esterification reaction between an acrylic acid (AA) and pentaerythritol (PER) catalyzed by PTSA-Silica is a series of reactions that will generate pentaerythritol monoacrylate(PEMA) and PEDA in succession and in some cases even pentaerythritol triacrylate (PETA). The final reaction equations can be described as follows:

64 $CH_2CHCOOH + C(CH_2OH)_4 \rightarrow PEMA + H_2O$

 $65 \qquad \text{PEMA} + \text{CH}_2\text{CHCOOH} \rightarrow \text{PEDA} + \text{H}_2\text{O}$

 $66 \qquad \text{PEDA} + \text{CH}_2\text{CHCOOH} \rightarrow \text{PETA} + \text{H}_2\text{O}$

67 Therefore, to obtain a high yield of PEDA products, it is necessary to systematically study the process 68 conditions of the esterification reaction. In this work, PEDA is synthesized by PTSA-Silica catalyzed the direct esterification of PER with AA using hydroquinone/anhydrous copper sulfate as the inhibitor and 69 70 toluene as the solvent. The procedure is briefly described as follows: A certain amount of pentaerythritol 71 (~ 30 g) and a small amount of hydroquinone -anhydrous copper sulfate (~ 1.2 g, w/w, 1:1) are 72 dissolved in toluene (~150 mL) in a three-necked flask (500 mL) equipped with a mechanical stirrer, a 73 thermocouple and a fractional distillation column (for separating water produced in the system). The 74 mixture is heated to a specific temperature, and then acrylic acid (\sim 33- 46 g) and PTSA-Silica (\sim 0.9-75 $\frac{4.8 \text{ g}}{1.8 \text{ g}}$ is added to the flask to start the reaction and maintain the reaction at the temperature for 50 \sim 300

76 minutes. After the reaction is completed, the reaction mixture is filtered to remove the catalyst. The 77 filtrate was cooled to room temperature and then separated into two layers (organic/water) by adding 78 saturated sodium chloride solution to it. The organic phase was collected, and its pH value was 79 adjusted to 7 by adding sodium hydroxide solution. The sodium salt generated was removed by water 80 washing, and the organic solvent was removed by reduced pressure distillation. The remainder was the 81 crude product of PEDA, and the purity was analyzed by high-performance liquid chromatography(HPLC). The specific analysis method is described in section 2.3. The yield of PEDA 82 83 can be calculated by the analysis result. We conduct a series of experiments in the flask in the temperature range of 373~403K, with the value of w_{cat} changing from 0.5% to 2.0 wt% and the value of 84 85 N_{AA}/N_{PER} from 2.1 to 2.9. Figure 1 presents a typical HPLC chromatogram of the crude product.



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Fig.1. HPLC chromatogram of the crude product (1-PEMA, 2-PEDA, 3-PETA).

In order to determine whether the main product obtained is the target product, it is necessary to
 obtain a small amount of pure product. The pure product of PEDA was obtained by utilizing column
 chromatograph (Eluent, V(CH₃OH)/V(CH₂Cl₂), 1:20) and its purity was analyzed by HPLC to be 99%.
 Figure 2 presents a typical HPLC chromatogram of the pure product.

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Fig. 2. HPLC chromatogram of the pure product.

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96 2.3. Analytic method

97 The concentrations of PEDA, PEMA, PETA in the sample are determined by high-performance liquid 98 chromatography (HPLC, Waters Breeze 1515) with refractometer 2414 as a detector. According to the 99 analysis results of HPLC, the yield of PEDA at a certain time can be calculated. The column used is 100 Sun Fire C₁₈ stainless steel (4.6mm×250 mm). The optimum operation conditions of HPLC are: column 101 temperature, 313K; flow phase, menthol(A)-potassium dihydrogen phosphate buffer solution (B, 0.2 102 mol·L⁻¹) (V_A : V_B = 10 : 90); flow rate, 1.0 ml·min⁻¹; sample volume, 10 µl.

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104 3. Results and discussion

3.1 Characterization of the PEDA product

106 The synthesized product of PEDA is characterized by FT-IR (NICOLET 6700 IR spectrometer), and the

107 result is shown in Figure 3. From Figure 3, bands with peak maximums at 3498 cm⁻¹(O-H stretching),

108 1727 cm⁻¹(C=O stretching), 1635 cm⁻¹(C=C stretching) and 1187 cm⁻¹(C-O-C stretching) all correspond

109 to motions associated with PEDA.





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3.2. Effect of Catalyst Concentration

The effect of catalyst concentration (w_{hat}) on the yield of PEDA was investigated by varying w_{cat} from 0.5wt% to 2.5wt% when the reaction conditions were as follow: *T*=393 K, N_{AA}/N_{PER} =2.7 and *t* = 240 mim. The relationship between the yield of PEDA and w_{cat} is presented in Figure 5. From Figure 5, it can be seen that the yield of PEDA increases from ~20% to ~ 52% when the value of w_{cat} changes from 0.5 wt% to 2.0 wt%. However, when w_{cat} >2.0 wt%, there no significant increase in yield of PEDA, this may be because the higher catalyst concentration will increase the chance of PEDA reacting with AA to generate PETA.



Fig. 5. The effect of the catalyst concentration on the yield of PEDA (*T*=393 K, *t*=240 min, N_{AA}/N_{PER} =2.7) 3.3 Effect of mole ratio of reactants When the reaction temperature is 393 K, and the value of w_{cat} is 2.0%, the effect of mole ratio of reactants on the yield of PEDA at a reaction time of 240 minutes was investigated by varying N_{AA}/N_{PER} from 2.1 to 2.9, and the results are shown in Figure 6. From Figure 6, it can be seen that the yield of PEDA increases with increasing in N_{L}/N_{L} until N_{L}/N_{L} =2.7 (vield 52.6%) and then decreases

144 PEDA increases with increasing in N_{AA}/N_{PER} until $N_{AA}/N_{PER} = 2.7$ (yield, 52.6%), and then decreases

- slightly. This may be because the higher concentration of AA is beneficial to the formation of PEDA,
- however, when the value of N_{AA}/N_{PER} is larger than 2.7, a portion of PEDA will be converted to PETA by reacting with AA.



(T=393 K, t=240 min, w_{cat} =2.0 wt%)

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152 3.4 Effect of reaction temperature and reaction time

153 The chemical reaction rate is strongly affected by the reaction temperature [21]. Therefore, the 154 effect of reaction temperature and reaction time on the yield of PEDA was investigated a period of 50 to 300 min when the reaction conditions are as follows: N_{AA}/N_{PER} =2.7, T =373 ~ 403 K and w_{cat} =2.0 wt%. 155 156 The results were shown in Figure 7. From Figure 7, the following conclusions can be drawn: (1) At the 157 same reaction time, the higher the temperature, the greater the yield of PEDA. For example, the yield of 158 PEDA at 240min increases from 28.9% to 64.5% when the temperature changes from 373 K to 403 K. 159 The reason is that the reactant molecules at higher temperature have higher energy and the probability 160 of collision between the molecules is larger; (2) At the same reaction temperature, the yield of PEDA increases with increaseing in reaction time for the lower temperatures (373K and 383K), however, 161 162 when the reaction temperature reaches or exceeds 393 K, the yield of PEDA increses with reaction time 163 until ~250 min, and then decreases. This may be because a small amount of PEDA turns into PETA 164 when the concentration of PEDA in the reaction mixture is sufficiently large.



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Fig.7. The effect of reaction temperature and reaction time on the yield of PEDA ($N_{AA}/N_{PER}=2.7$, t=240 min, $w_{eat} = 2.0$ wt%)

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169 **5. Conclusions**

170 In this work, pentaerythritol diacrylate (PEDA) is synthesized by reacting pentaerythritol (PER) 171 with acrylic acid (AA) using PTSA-Silica as catalyst and toluene as solvent. The product of PEDA is 172 purified by chromatography, and the purified product is gualitatively analyzed by Fourier transform 173 infrared spectrometer (FT-IR) and nuclear magnetic resonance carbon (¹³C-NMR)infrared 174 spectroscopy. The results show that there are two alcoholic hydroxyls in the formula of the product, 175 indicating it is the target product PEDA. The effects of various operating conditions such as the catalyst 176 concentration(w_{cat} 0.5~2.5wt%), the reaction temperature (T, 373~403 K), the reaction time (t, 50~300 177 min), and the reactants mole ratios (N_{AA}/N_{PER} , 2.1~2.9) on the yield of PEDA are investigated. The 178 results show that the yield of PEDA increases with increasing in w_{cat} up to 2.0 wt%, and then tends to 179 be gentle, and the highest yield of PEDA reaches to 64.5% when the operation conditions are as 180 follows: N_{AA}/N_{PER} =2.7, T=403 K, t =240 min and w_{cat} =2.0 wt%.

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